

REMOVAL OF ORGANICS FROM COLOURED WATER PHASE TWO REPORT

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REMOVAL OF ORGANICS FROM COLOURED WATER - PHASE TWO REPORT

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SUMMARY

I OBJECTIVE

To investigate the production of disinfection by-products during the treatment of coloured water and to define suitable, cost effective, methods for their removal or control with due regard to other water quality determinands, such as colour, iron, manganese and aluminium.

II REASONS

The presence of disinfection by-products in drinking water derived from coloured sources may pose a health risk to the consumer and exceed regulated water quality criteria. Dissolved air flotation and 2 stage filtration has been identified as the most likely process to be used for treatment of upland coloured water; this process requires investigation and optimisation with respect to the control of the trace organics of concern.

III CONCLUSIONS

- (i) Pre-chlorination increases disinfection by-products.
- (ii) Interfiltration chlorination increases disinfection by-products; for manganese removal it may be possible to discontinue chlorination when the filter is "conditioned".
- (iii) Low pre-ozonation doses do not adversely affect disinfection by-products, and can result in small savings in coagulant.
- (iv) High pre-ozonation doses disrupt the coagulation/flocculation process, resulting in poor quality final water.
- (v) When ozonating waters containing manganese, the manganese may be oxidised to a form that is difficult to remove by conventional filtration.

(vi) . Interfiltration or post-treatment ozonation reduces disinfection by-products.

IV RECOMMENDATIONS

Pre-oxidation should not be used unless considered necessary (e.g. for algal removal), and where possible ozone should be considered in preference to chlorine.

The interfiltration chlorine dose for manganese removal should be kept as low as possible; to minimise by-product levels the secondary filters should not be used to provide residence time for disinfection.

Where there are high levels of disinfection by-products, these can be reduced by using ozone instead of chlorine after the first stage of rapid gravity filtration. In this event, site specific studies should be carried out to determine how ozonation can be achieved without adversely affecting manganese removal.

V RESUME

A series of tests, examining the application of ozone or chlorine at various points within a three stage treatment stream, has been carried out as the second phase of a 3 phase experimental programme. The details and results of each test are provided and conclusions have been drawn.

CONTENTS

		PAGE
SECTION 1 -	INTRODUCTION	1
SECTION 2 -	EXPERIMENTAL DETAILS	2
2.1	ADDITIONS AND ALTERATIONS TO THE PILOT PLANT	. 2
2.1.1	Ozone Generator	2
2.1.2	Ozone Contactors	2
2.1.3	Additional Secondary RGFs and Modified Pipework	3
2.1.4	Streaming Current Detectors	3
2.2	EXPERIMENTAL PROGRAMME	3
2.3	SAMPLING AND ANALYSIS	7
2.4	PILOT PLANT CONTROL AND OPERATION	7
SECTION 3 -	RESULTS .	9
3.1	RAW WATER QUALITY	9
3.2	CORRELATIONS BETWEEN DETERMINANDS	10
3.2.1	uv vs. TOC	10
3.2.2	AOX vs. THMs	10
3.2.3	AOX vs. Mutagenic Activity	10
3.2.4	THMs vs. Chlorine Demand	11
3.3	EFFECT OF TREATMENT ON INORGANIC DETERMINANDS	11
3.3.1	Effect of Prechlorination	11
3.3.2	Effect of Interfiltration Chlorination	11
3.3.3	Effect of Preozonation and Ozonation of Raw Water	13
3.3.4	Effect of Interfiltration Ozonation	14
3.3.5	Effect of Dual Point Ozonation	13
3.4	BACTERIOLOGICAL QUALITY OF TREATED WATER	14
3.5	EFFECT OF TREATMENT ON ORGANIC DETERMINANDS	14
3.5.1	Effect of Pre and Interfiltration Chlorination	14
3.5.2	Effect of Raw Water Ozonation	14
3.5.3	Effect of Preozonation	15
354	Effect of Interfiltration Ozonation	15

	3.3.5	Effect of Dual Point Ozonation	1
	3.6	EFFECT OF TREATMENT ON DISINFECTION BY-PRODUCTS	1
	3.6.1	Effect of Prechlorination	1
;	3.6.2	Effect of Interfiltration Chlorination	1
	3.6.3	Effect of Preozonation and Ozonation of Raw Water	2
	3.6.4	Effect of Interfiltration Ozonation	2:
	3.6.5	Effect of Interfiltration Ozonation pH	23
	3.6.6	Effect of Dual Point Ozonation	23
		CONCLUSIONS AND RECOMMENDATIONS	24
SECT	rion 5 -	REFERENCES	26
SECT	CION 6 -	ACKNOWLEDGEMENT	27
APPE	NDIX A -	OZONE CONTACTORS DETAILED DESCRIPTION	41
APPE	NDIX B -	- TABLES OF RESULTS	43

SECTION 1 - INTRODUCTION

This report details the results obtained from running a three stage dissolved air flotation (DAF) water treatment pilot plant for the removal of organics from upland water. It contains all the results obtained from the second phase of a three phase experimental programme. A full description of the pilot plant, its operation, and the three phases of the experimental programme are given in the First Interim Progress Report (1). The results obtained from the first part of the experimental programme are detailed in the Phase One Report (2).

Because of the nature of the programme and large number of results involved, operational details and tables of results have not generally been included within the main body of this report; details of each experiment together with all results are supplied as appendices.

SECTION 2 - EXPERIMENTAL DETAILS

2.1 ADDITIONS AND ALTERATIONS TO THE PILOT PLANT

For phase II of the experimental programme, a number of additions and alterations were made to the pilot plant. These included the addition of ozone equipment, streaming current detectors, two extra secondary rapid gravity filters (2° RGFs) and some pipework modifications.

2.1.1 Ozone Generator

The ozone generator was an Ozobloc O.C.2. generator supplied by Ozotech Ltd. The generator contained two ozonation tubes, and could generate a maximum of 38 g/hr of ozone. The generator was supplied with compressed air from a Hydrovane "5 puts" rotary vane compressor.

Ozone from the generator could be supplied to any of three ozone contactors (described below), or to the thermal ozone destructor. The destructor allowed the dosing of very low quantities of ozone, whilst maintaining a reliable ozone output from the generator; surplus ozone being fed to the destructor. A flowsheet for the ozone equipment is shown in figure 1.

2.1.2 Ozone Contactors

Three ozone contactors were installed for phase II; they were designed by WRc and constructed by Portobello Fabrications Ltd. Each contactor consisted of a base section, including viewing window, beneath a stainless steel column (figure 2). Three nominal sizes of column were used one for each contactor: 4", 6", and 8". A more detailed description of the contactors is given in Appendix A.

It was possible to use any single contactor, or two in series, to ozonate either the raw water, or the primary (1°) RGF filtrate. If required, the raw water and 1° RGF filtrate could be ozonated simultaneously using two separate contactors.

2.1.3 Additional Secondary RGFs and Modified Pipework

Two extra 2° RGFs, identical to those used in phase I, were installed at the beginning of phase II. There were also a number of alterations made to the pipework, which are shown in figure 3. These alterations made it possible to:

- (i) Run two 2° RGFs from the same 1° RGF.
- (ii) Run both 1° RGFs from the same DAF.
- (iii) Ozonate the feed to stream B 2° RGFs.
- (iv) Ozonate the combined filtrates from RGFs A2, B2 and B3

The description of the experimental programme (section 2.2 below) details how these options were used.

2.1.4 Streaming Current Detectors

During phase II, two streaming current detectors (SCDs) were installed; one on each stream. At first, these were used to monitor and record. But later on they were used to control the coagulant dose.

2.2 EXPERIMENTAL PROGRAMME

The objective of phase II was to investigate the use of ozone and chlorine as pre- and inter-filtration oxidants. The flow scheme is shown in figure 3. The experimental programme was divided up into a number of trials, described below. The filter nomenclature used in figure 3 has been kept throughout the description of each trial.

Trial la. Prechlorination

During this trial both DAFs were run, with hypochlorite dosed to stream B before the flocculators to give a free residual after the DAF. The ferric dose ranged from 3.7 to 4.2 mg/l, being approximately equal for each stream. The prechlorine dose ranged from 1.30 to 1.76 mg/l, which

was sufficient to give a free residual after the DAF ranging from 0.19 to 0.35 mg/l. Water from DAF A fed RGF A1, and then RGF A2; water from DAF B fed RGF B1, and then RGF A3. Both 2° RGFs continued to use the sand that had been used in phase I.

Trial 1b. Inter Filtration Chlorination

During this trial only one DAF and one 1° RGF were run; the ferric dose was kept in the range 4.1 to 4.5 mg/l. Water from DAF A fed RGF Al, and then split to feed RGFs A2 and A3. The chlorine dose to RGF A2 was kept constant to provide a residual of 0.1-0.2mg/l after the filter. The dose to RGF A3 was varied to give a range of free chlorine residuals after the filter; the chlorine dosed ranged from no chlorine, to enough to provide a free residual of 0.5 mg/l after allowing the filtrate to stand for 30 minutes. The sand in both 2° RGFs was the same as had been used throughout phase I.

Trial 2a. Raw Water Ozonation

During this trial, raw water was passed through one of the ozone contactors, and then sampled without further treatment. The applied ozone dose was varied from 0.5 to 9 mg/l, and the contact time between 1.5 and 10 minutes. Variations in ozone dose were achieved by altering the concentration of ozone in the ozonated air stream (by adjusting the power applied to and the gas flowrate through the ozone generator), and by the division of ozone flow to the contactor and destructor. Variations in contact time were achieved by adjusting the raw water flow and the size of the ozone contactor.

Trial 2b. Preozonation

During this trial, stream A was the control stream and the raw water feed for stream B was passed through one of the ozone contactors before addition of coagulant. The ozone dose was varied, between 0.5 and 6 mg/l; a contact time suited to a particular ozone dose was chosen. During this trial, the ferric doses were varied from 2.9 to 5.5 mg/l.

However, for most of the trial, the ferric doses in both streams were equal. For the last run, the ferric dose to the ozonated stream was intentionally set lower than that to the control stream. The flowsheet for the pilot plant was exactly the same as in trial la, except the trial stream was pre ozonated, instead of pre chlorinated. The sand in both 2° RGFs was the same as had been used throughout.

Trial 3a. Inter Filtration Ozonation - Fixed pH

At the beginning of this trial, the two new 2° RGFs (B2 and B3) were commissioned. The old sand from RGF A2 was transferred to RGF B3, and new sand was placed in RGFs A2 and B2. Only one DAF (A) was run during this trial. The caustic for pH correction before the 1° RGFs was dosed into the DAF outlet after which the stream was split to feed RGFs A1 and B1. These in turn fed RGFs A2 (new sand) and A3 (old sand) or RGFs B2 (new sand) and B3 (old sand) respectively.

For the first five runs of this trial, filtrate from RGF Al was dosed with caustic and chlorine before being split to feed RGFs A2 and A3. For the last three runs only caustic was dosed prior to the split. RGF A3 was fed with chlorinated water and RGF A2 was fed with non oxidised water; both operated at pH 9. This was done in order to test how long manganese removal could be maintained without the use of an oxidant. The sand in RGF A2 had been new at the beginning of this trial, and had been conditioned with chlorinated water for six weeks before stopping its chlorine dose.

For the first half of this trial, all the filtrate from RGF B1 was passed through the small ozone contactor before feeding RGFs B2 and B3 thus providing a comparison of new and old sand. However, during the second half of this trial, the filtrate from RGF B1 was split, half going to the ozone contactor to feed RGF B3, the other half feeding RGF B2 directly. Ozone was then applied to the base of RGF B2, as shown in figure 4. This arrangement was intended to give counter current contact of ozone with water within the bed of sand to encourage deposition of MnO_2 . However, the pressure drop across the sand was too great, and the result was that

both ozone and filtrate left in the filtrate outlet. The effect of this was to give a very short inefficient contact between ozone and non oxidised 2° RGF filtrate.

The above arrangement gave an ozone contact time prior to the 2° filtration of 8 minutes during the first half of the trial and 15 minutes during the second. During the second half of the trial, the un-oxidised filtrate from RGF B2 was contacted with ozone for a very short period estimated to be 15 seconds.

During each half of the trial, the ozone dose was varied between 0.3 and 5.0~mg/l, and the ferric dose was controlled between 2.1 and 4.1 mg/l. During the second half of the trial, the ferric dose was controlled by an SCD at between 2.1 and 2.6 mg/l.

Trial 3b. Inter Filtration Ozonation - Fixed Dose and Contact Time, Variable pH

During this trial, the pilot plant was run as in the second half of trial 3a (i.e. RGF B2 was ozonated directly), except that the caustic dose before RGF A3 and prior to ozonation was varied to vary the filtrate pH. The pH of RGF A2 filtrate was maintained at pH 9, with no chlorine dosed to this filter or B2 and B3. The ferric dose during this trial was controlled within the range 1.5 to 2.0 mg/l by an SCD.

Trial 3c. Ozone Disinfection (Post ozonation)

During this trial, the pilot plant was run as in trial 3b, except that RGFs B2 and B3 were fed with unozonated water. Thus RGFs A2, B2 and B3 were all fed with unoxidised water at pH 9. The filtrates from these three filters were combined, and fed to the ozone contactor at a contact time of 8 minutes. RGF A3 was fed with chlorinated water at pH 9, as a control. The ferric dose was controlled to 1.7 and 1.9 mg/l by an SCD.

Trial 4. Dual Point Ozonation

During this trial both DAFs were operated; DAF A was the control and DAF B the trial. Ozone was applied to the trial stream raw water at a contact time of 3 minutes before coagulation; DAF A fed RGFs A1, A2 and A3, and DAF B fed RGFs B1, B2 and B3. The trial stream 2° RGFs were fed with ozonated 1° filtrate; the contactor had a contact time of 8 minutes. The trial stream ferric dose was controlled by an SCD between 1.5 and 2.1 mg/l. However, the control stream SCD malfunctioned at the beginning of this trial, so the control stream ferric dose was manually controlled between 1.6 and 2.5 mg/l.

2.3 SAMPLING AND ANALYSIS

With the exception of chlorine residual measurement, the sampling and analysis during phase II were identical to those during phase I. Details of these analyses are given in the first interim progress report (1).

During phase II, it became apparent that oxidised forms of manganese were giving serious errors in the measurement of free chlorine using DPD powder, especially when analysing ozonated waters. This can be corrected by using 'steady fac' tablets, available from Pallintest Ltd. These work by quenching chlorine in the water, to give the reading attributable to oxidised manganese. This can then be subtracted from the overall reading, to give the reading for free chlorine. These tablets were used from the beginning of trial 3b to the end of the experimental programme.

2.4 PILOT PLANT CONTROL AND OPERATION

In addition to the operational problems and observations encountered during phase I (2), the following occurred during phase II.

(i) Flotation in Flocculators After Pre Ozonation

Because the ozone contactors have a liquid depth of almost 5m, water is effectively contacted with ozonated air at 50kPa pressure. Thus, when water from the contactors flows into the

flocculators at atmospheric pressure, it may be supersaturated with air. When this air comes out of solution, it causes floc to rise to the top of the water in the flocculators and form a float. At high ozone doses, ozone residual would also degas resulting in high concentrations of ozone in the air above the flocculator. In an attempt to lessen this effect, two contactors were always run in series when pre ozonation was practised. Ozone was fed to the first contactor, and the second was used to allow some degassing and decay. Unfortunately, a column is not the optimum shape for degassing, and there were still some problems caused by float in the first flocculator. investigate if this affected the treatment process, one run during trial 2b was carried out where air was contacted with the raw water before coagulation. The results indicated that although flotation took place in the flocculators it did not affect the quality of the final water (Appendix B, trial 2b, ozone dose = 0.0 mq/1).

(ii) Very Long pH Stabilisation Periods

On a number of occasions, control of filtration pH failed for a short period, (e.g. if dosing pumps failed over the weekend). After these periods, it took a number of hours for 1° RGFs to reach the correct pH, and the old-sand 2° RGFs could take two days. This is in contrast to the residence times which are about 10 minutes and 5 minutes respectively. The reason for this is not clear but it may be that the surface of the conditioned sand was acting as a buffer by some unidentified ion exchange phenomena.

SECTION 3 - RESULTS

Unless indicated otherwise, the curves drawn in all figures are the interpretation of the operator.

3.1 RAW WATER QUALITY

Figures 5 to 10 show plots of raw water quality against time. Results from both phase I and phase II are included, so a comparison can be made between the raw water quality for each phase.

Figure 5 shows very clearly the annual cycle for uv absorbance and colour, with maximum uv absorbance and colour in the Autumn (November/December), and minimum uv absorbance and colour in the Spring (May/June).

The plot for turbidity, in figure 6, is far more erratic than the plots seen in figure 5. This shows that turbidity is more influenced by short term weather conditions (increasing after heavy rain or violent winds), than by the annual variations in raw water quality.

The plot for pH in figure 6 seems to follow an annual cycle. From Autumn through to Summer (November through to September), the pH gradually increases, but during October, there was a drop in pH.

Figure 7 shows that changes in the raw water iron concentration follows the same trend as the raw water colour. However, changes in the aluminium concentrations seem to coincide with changes in pH, with low pH coinciding with high aluminium. It would therefore seem likely that a large proportion of the iron is closely bound with humic substances, but that aluminium is not and can therefore be leached from the soil more effectively by water at low pH. The plot for raw water manganese shows much less variation with time. There seem to be two plateaus, with the concentration remaining constant for most of the year, but changing during the summer.

Figures 8 and 9 show that both TOC and chlorine demand follow a similar pattern to colour and uv absorbance, but the peak chlorine demand is earlier.

The plots for THMs and AOX formed during hand chlorination of raw water, figure 10, do not show clear seasonal trends. THM potential appears to decrease through the final period whereas AOX potential appears to increase.

3.2 CORRELATIONS BETWEEN DETERMINANDS

3.2.1 uv vs. TOC

Figure 11 shows a plot of uv absorbance against TOC. It can be seen that there are two correlations for the raw water with slope depending on whether or not it had been ozonated. This is because ozone is effective at reducing uv absorbance, but has very little effect on TOC. This stresses the point that, although uv absorbance can be a very good surrogate for TOC, there are times (i.e. when ozone is involved) when it is not. The correlation for both data sets is good (r = 0.96) for ozonated and (r = 0.87) for unozonated.

The results for filtered samples did not show the same degree of difference between ozonated and unozonated samples. This is because the results for uv absorbance for ozonated filtrates were increased by the presence of colloidal manganese in the samples.

3.2.2 AOX vs. THMs

Figure 12 shows that there is a positive correlation (r = 0.68) between AOX and THMs, but it is not a useful correlation due to the high scatter.

3.2.3 AOX vs. Mutagenic Activity

Figure 13 shows that there is a positive correlation (r = 0.74) between AOX (below $40\mu g/l$) and TA 100 mutagenic activity, and weaker correlation

(r = 0.61) between AOX and TA 98 activity. There is, however, little correlation between high AOX levels (<70 $\mu g/l$) and mutagenic activity.

3.2.4 THMs vs. Chlorine Demand

Figure 14 shows a positive correlation (r = 0.62) between chlorine demand and THMs, but the scatter makes it impossible to use the correlation in a predictive way.

3.3 EFFECT OF TREATMENT ON INORGANIC DETERMINANDS

3.3.1 Effect of Prechlorination

Prechlorination at a dose of 1.3-1.8 mg/l had no effect on inorganic determinands.

3.3.2 Effect of Interfiltration Chlorination

Variations in interfiltration chlorine dose up to 1.3 mg/l did not produce discernible variations in metals or turbidity. This was considered to be due to the effectiveness of the 1° RGFs in removing iron, aluminium and turbidity.

During the last three months of the experimental programme it was possible to compare the performance of a 2° RGF fed with chlorinated water, with one fed with unchlorinated water. Two runs during this period produced relatively high aluminium and iron concentrations (0.1-0.2 mg/l) in the 1° filtrate due to poor pH control. The chlorinated 2° RGF was then capable of removing about 50% of this iron, but none of the aluminium. The unchlorinated 2° RGF could not remove any iron.

The unchlorinated 2° RGF was capable of removing manganese from about 0.2 mg/l in the 1° filtrate down to about 0.01 mg/l over a three month period (for the second half of this three month period, the filter was

not backwashed, thus ensuring no chlorinated water was fed to the filter). However, during one run, the 2° filtrate pH dropped to about 7.2; at this pH, chlorine was required for effective manganese removal.

3.3.3 Effect of Preozonation and Ozonation of Raw Water

The effect of preozonation was dependent on ozone dose. At low doses (up to 2 mg/l), preozonation had little effect on metals or turbidity. At higher doses, the concentration of iron, aluminium and turbidity in the final water increased. However, ozonation resulted in some manganese removal by the DAF and the 1° RGF but the concentration of manganese in the final water was slightly higher in the preozonated stream, (it was still 20 μ g/l or less). The effect of ozone dose on 1° RGF manganese removal is shown in figure 15.

Figure 16 shows colour generated by adding DPD (No. 1) to raw water, after passage through the ozone contactor, plotted against ozone dose. DPD was used to measure ozone residual concentration in the water but the DPD was probably affected more by manganese than by ozone, it is therefore considered to be more a measure of oxidised forms of manganese. It can be seen in figure 16 that low ozone doses result in virtually no oxidised manganese or ozone residual, but that at higher ozone doses where there would be an expected ozone residual, (greater than 2.5 mg/l) manganese becomes oxidised. Once oxidised, some of this manganese can be removed by coagulation, dissolved air flotation and rapid gravity filtration at pH 6.5, as shown previously by figure 15.

Figure 16 suggests that at low doses, ozone is rapidly depleted by reacting with organic matter and there is little or no ozone residual and the coagulation process is unaffected. At higher doses, where there will be free ozone, inorganic matter also becomes oxidised and the coagulation/flocculation chemistry is disturbed. High preozone doses thus result in poorer final water quality particularly in respect of iron, aluminium and turbidity.

3.3.4 Effect of Interfiltration Ozonation

As with interfiltration chlorination, if the iron residual in the 1° filtrate was high, then ozonation before 2° filtration enabled the removal of some (~50%) of that iron by the 2° filters.

Interfiltration ozonation appeared to oxidise manganese present in the 1° filtrate but the 2° filters were not capable of removing more than about 50% of this manganese; the remaining manganese was present in a form which significantly contributed to the colour and turbidity of the water. This increased the turbidity of the final water by up to 0.8 NTU, and the colour by up to 14 Hazen. Only some of this manganese (~50%), and associated colour, could be removed by filtration through a 0.45 μ m membrane.

When the water containing manganese was ozonated, the manganese appeared to be oxidised to manganese dioxide very quickly and as a result formed a colloidal suspension which was not readily removed by rapid gravity filtration. This contrasts with the process which occurs with chlorination, where the oxidation process is much slower and is catalysed by the manganese coated sand surface; oxidation occurs at the surface of the sand, and results in the deposition of the manganese dioxide on the filter as it forms.

When one of the 2° filters was run with application of ozone to the base of the filter (see figure 4), manganese was successfully removed, not by ozonation, but by the combination of high pH and manganese coated sand. The non-chlorinated, non-ozonated, 2° RGF showed that high pH and sand alone were effective for manganese removal.

The chemistry of manganese removal is very complex, and is dependant on a number of factors, including redox potential, hardness/alkalinity, and pH. It is therefore not necessarily true that observation at Clough Bottom would be repeated at other sites.

3.3.5 Effect of Dual Point Ozonation

The overall effect of dual point ozonation (pretreatment and interfiltration) on inorganic determinands is exactly the same as the combined effects of ozonation at each point.

3.4 BACTERIOLOGICAL QUALITY OF TREATED WATER

The bacteriological quality of the water after hand chlorination was not affected by the use of ozone at any point in the treatment process. The water disinfected by ozone alone was also of the same, acceptable, bacteriological quality that resulted from chlorination.

3.5 EFFECT OF TREATMENT ON ORGANIC DETERMINANDS

3.5.1 Effect of Pre and Interfiltration Chlorination

Both pre and interfiltration chlorination resulted in a slight reduction (no more than 10%) in final water colour and uv absorbance. Neither pre nor interfiltration chlorination had any effect on TOC.

3.5.2 Effect of Raw Water Ozonation

Figures 17 to 19 show plots of true colour, true uv absorbance and TOC respectively, plotted against ozone dose. The results were obtained at a number of different contact times.

Figure 17 shows that ozone doses up to about 2.3 mg/l resulted in a reduction in true colour proportional to ozone dose. True colour was reduced by approximately 4 Hazen for every mg/l of ozone dosed. Above doses of 2.5 mg/l, no further reduction in colour was achieved, giving a minimum colour of about 14 Hazen. This colour reduction is very much less than reported from previous trials (3), where reductions of 10 Hazen for every mg/l ozone dosed, and minimum colours of 5 Hazen are reported. It is probable that the manganese is being oxidised (figure 16) into a colloidal form which is not removed by the 0.45 µm membranes used when

measuring true colour; thus the organic colour may have continued to be reduced by ozone doses above 2.5 mg/l but this was counteracted by an increase in inorganic colour due to manganese oxidation.

Figure 17 shows that colour removal was independent of contact time.

Figure 18 shows that ozone reduced uv absorbance and that the rate of reduction decreased with increasing dose. As with colour, uv reduction was independent of contact time.

Figure 19 shows that ozone dose had no effect on TOC concentration.

3.5.3 Effect of Preozonation

Figures 20, 21 and 22 show the effect of preozone dose on final water colour, uv absorbance and TOC respectively. During these runs, the coagulant dose of the preozonated stream was equal to the coagulant dose of the control stream. Ozone doses up to about 2 mg/l resulted in a reduction in final water colour and uv absorbance (fig. 20, 21); however, ozone doses greater than about 4 mg/l resulted in a deterioration in final water colour and uv absorbance. This is considered to be due to ozone interfering with the flocculation/coagulation chemistry. The results in figure 22 indicate that preozonation had little or no effect on the concentration of TOC in the final water.

At the end of this trial, one run was carried out where 1 mg/l of ozone was dosed to the raw water of the trial stream. The trial stream ferric dose was then reduced until the final water colour of the trial stream equalled that of the control stream. This enabled a reduction in ferric dose of 20%, from 4.0 to 3.2 mg Fe/l.

3.5.4 Effect of Interfiltration Ozonation

Interfiltration ozonation resulted in an increase in final water colour, this was considered to be due to the production of colloidal manganese. However, when ozone was applied to water from which manganese had already

been removed (i.e. direct application of ozone to the base of a 2° RGF, or during the disinfection trial), the final water colour was reduced from 2 or 3 Hazen down to 1 Hazen.

Figure 23 shows final water uv absorbance plotted against interfiltration ozone dose. It can be seen that increasing ozone doses resulted in a reduction in uv absorbance. All the points lie close to the curve, including those derived from direct ozonation to the base of the filter thus showing that only a short contact time was required. The curve is similar to the curve observed for raw water ozonation (figure 18), and it would seem that little benefit is obtained for uv absorbance reduction at ozone doses higher than 2 mg/l. However when ozone was applied to final water during the disinfection trial, lower final water uv absorbances (about 1.0 m-1) were obtained. This may have been because there was no colloidal manganese present which could have interfered with the measurements in figure 23.

Figure 24 shows a plot of the difference between the trial stream final TOC and the control stream final TOC. From this figure it can be seen that interfiltration ozone appeared to increase TOC removal by up to $0.5\,$ mg/l at ozone doses over 2 mg/l. There is also an indication that removal increased with increasing contact time.

The trials investigating ozonation pH indicated that pH had no consistent effect on colour, uv absorbance or TOC oxidation by ozone.

3.5.5 Effect of Dual Point Ozonation

The effect of dual point ozonation was found to be the same as combining the separate effects of pre and interfiltration ozonation.

3.6 EFFECT OF TREATMENT ON DISINFECTION BY-PRODUCTS

3.6.1 Effect of Prechlorination

Although prechlorination reduced the chlorine demand of the treated water it produced significant increases in total chlorine consumption and

disinfection by-products. These are summarised in table 1, which shows percentage increase in each determinand in the prechlorinated stream compared to the control stream. Chlorine consumption is the total chlorine dosed to the raw water, before the 2° filter and in the lab, minus the free residual after 30 minutes of hand chlorination. The results for chlorine consumption and total THMs are an average from two runs, those for AOX and mutagenic activity are from a single run.

Table 1 - Percentage Increase in Disinfection By-Products

Determinand	% Increase
Cl Consumption	180
Total THMs	125
AOX	40
TA 98 Mutagenic Activity	40
TA 100 Mutagenic Activity	70

The increase in chlorine consumption appears to have increased THM production to a greater extent than AOX or mutagenic activity.

3.6.2 Effect of Interfiltration Chlorination

Generally, the sum of the chlorine consumed during 2° filtration and the chlorine consumed during the laboratory chlorination of the 2° filtrate was greater than the chlorine consumed during the laboratory chlorination of the 1° filtrate. In both cases chlorination conditions were similar; the final residual was 0.5 mg/l, the pH was 9.0, and the contact time was c 30 minutes (c5 minutes contact in the filter plus 30 minutes in the laboratory, or 30 minutes in the laboratory).

When no chlorine was dosed prior to the 2° filter, the chlorine consumption of the 1° filtrate and the 2° filtrate was comparable, indicating that, on this occasion, the chlorine demand of the water was not greatly affected by passage through the 2° filter. However, when the interfiltration dose was increased, to give a higher free residual after the 2° filter the total consumption of chlorine also increased, despite a

reduction in the chlorine dose required to give a residual of 0.5 mg/l after 30 minutes in the laboratory. The greater the proportion of the total chlorine dose that was applied before the 2° filters, the greater was the increase in total consumption of chlorine and this increase was reflected in increased THM production.

Figures 25 and 26 show the increased chlorine consumption and total THMs respectively, plotted against 2° filtrate free chlorine residual; the higher residuals reflect a greater proportion of the chlorine dose applied before the 2° filters. The increases shown are far greater than would be expected by the relatively small increase in contact time due to passage through the 2° filter (~5 minutes).

These observations are supported by results obtained during the last three months of the experimental programme, when 14 runs were carried out where a chlorinated 2° filter was compared with an unchlorinated 2° filter. A summary of the results for total consumption of chlorine and total THMs is given in table 2.

Table 2 - Comparison of chlorinated and un chlorinated 2° filters

Chlorinated 2° filter	Un chlorinated 2° filter
- 98.2 44.9	12.6 13.4
61.4 59.9	11.0 19.8
0.07 0.014	0 0
	98.2 44.9 61.4 59.9

inclusive of hand chlorination

Table 2 shows that there were large differences in both total chlorine consumption and THM production between the chlorinated 2° filtrate and the 1° filtrate, despite low chlorine doses applied to the 2° filter (as

² after hand chlorination

shown by the free residual). The results for the chlorinated 2° filter in table 2, and those in figures 25 and 26 indicate that chlorine consumption and the production of by products is increased during passage through the 2° filter, it may be that the sand surface is catalysing the reaction taking place, resulting in the increases.

In slight contrast to a previous observation, table 2 shows that there were increases in chlorine consumption and THMs when chlorine was applied only after the 2° filter. Although these increases were small, the differences were statistically significant (at the 99% confidence level in the case of chlorine consumption, and at the 90% confidence level in the case of THMs). The reason for these increases is not clear.

Table 3 - Comparison of Chlorinated and Unchlorinated 2° Filter AOX

	Mean (μg/l)	Std. Dev. (µg/l)	No. of Points
Non Hand Chlorinated Chlorinated 2° Filter	28.1	7.7	5
Hand Chlorinated 1° Filter Un Chlorinated 2° Filter Chlorinated 2° Filter	26.8 30.0 31.2	3.6 3.7 5.9	7 6 7

Table 3 shows a summary of AOX results obtained over the same period. There was no significant difference between the results in table 3 (at the 95% confidence level). It therefore seems that THM production was more sensitive than AOX to chlorine consumption. This was also true of the prechlorination trial.

Table 4 - Comparison of Chlorinated and Unchlorinated 2° Filter
Mutagenic activity after hand chlorination

MUTAGENIC ACTIVITY MEASURED IN HAND CHLORINATED FILTRATE	Mean	Mean (3lope) Std. Dev.(Slop		v.(Slope)	No. of	Points
IN HAND CHECKINATED FIBINATE	TA 98	TA 100	TA 98	TA 100		
Un Chlorinated 2° Filter	7.06	33.06	1.2	0.7	. 3	
Chlorinated 2° Filter	7.53	35.67	0.5	2.9	3	

Table 4 shows a summary of mutagenic activity results obtained over the same period. The table shows that, as for AOX, there was no significant difference in mutagenic activity between the hand chlorinated filtrates from the chlorinated 2° filter and the unchlorinated 2° filter.

3.6.3 Effect of Preozonation and Ozonation of Raw Water

Raw water ozonation had no measurable effect on chlorine demand or total THMs, as shown by figures 27 and 28.

Figures 29, 30 and 31 show chlorine consumption, total THMs, and AOX, respectively, plotted against preozonation ozone dose. The corresponding values for the control stream are shown to indicate how the raw water quality changed during the trial.

From figures 29 and 30, it can be seen that there was no reduction in chlorine consumption or total THMs as a result of preozonation, and that if anything, there was a slight increase. However, figure 31 shows that there was a reduction in AOX with preozonation, although there is too much scatter in the figure to be able to tell how dependant this reduction was on ozone dose.

Table 5 shows the percentage reduction in mutagenic activity in the final chlorinated water resulting from a preozonation dose of 4 mg/l. The table shows that preozonation reduced mutagenic activity, as well as AOX.

Table 5 - Percentage Reduction in Mutagenic Activity with Pre Ozonation

Activity	% Reduction
TA 98	54
TA 100	24

3.6.4 Effect of Interfiltration Ozonation

There were a number of problems with measuring chlorine consumption of waters ozonated before 2° filtration, due to oxidised forms of manganese interfering with chlorine residual measurement. However, from the disinfection and direct ozonation runs, where manganese was removed before ozonation, it was apparent that interfiltration or post ozonation had little effect on chlorine consumption.

THM production was measured in samples collected after the 1° filters (before ozonation) and after the 2° filters (after ozonation) (similarly samples were collected before and after postozonation), so it was possible to examine the effect of ozonation directly without the need to compare the trial stream with the control stream.

Figure 32 shows a plot of percentage decrease in total THMs between 2° and 1° filtrates plotted against ozone dose (i.e. a high value on the graph corresponds to a low value for THMs). There are five data sets included, corresponding to 8 minutes ozone contact time followed by rapid gravity filtration with new or old sand; 15 minutes ozone contact time followed by rapid gravity filtration; direct application of ozone to a filter; and ozone disinfection of 2° filtrate.

From figure 32, it can be seen that there was a reduction in total THMs with ozonation, but that this reduction was not a function of ozone dose. It can also be seen that there was no difference in filtrates from the new or old sand. Although care must be taken in interpreting this data, the postozonation disinfection runs resulted in the greatest reduction in

THM production, and the direct ozonation runs resulted in the smallest reduction. There was, however, no significant difference in THM production between the 8 and 15 minutes contact times.

Since there is no clear effect of ozone dose in figure 32, it may be that only a small ozone dose was required for THM reduction, higher doses could have had a counteractive effect.

Figure 33 shows a similar plot of percentage decrease as used in figure 32, but for AOX against ozone dose. The five data sets in the figure are the same as for figure 32. As with THMs, there was a definite reduction in AOX resulting from ozonation and again there was no marked effect of ozone dose.

Table 6 gives a summary of the results for mutagenic activity. The results are expressed as the percentage difference (reduction) between the trial stream and the control stream hand chlorinated final waters.

Table 6 - % Reduction in Mutagenic Activity (compared to control stream)

OZONE DOSE (mg/l)	CONTACT TIME (mins)	TA 98	TA 100
0.4	8	51	54
5.0	8	96	72
5.0	15	82	73
5.0	DIRECT	76	46

Table 6 shows that interfiltration ozonation resulted in large reductions in the generation of mutagenic activity during subsequent hand chlorination. It also indicates that increasing the ozone dose above 0.4 mg/l was more beneficial. The result for TA 100 activity after direct ozonation is significantly lower (i.e. greater activity) than the other results at the same ozone dose. This sample also produced an extremely high AOX result (50% greater than the raw water). It would therefore seem that a greater contact time, and therefore better utilisation of the ozone, is required than is provided by direct ozonation.

3.6.5 Effect of Interfiltration Ozonation pH

Figures 34, 35 and 36 show total THMs respectively plotted against ozonation pH. Figure 34 shows results obtained by taking 1° filtrate, ozonating at various pHs and then adjusting the pH to 9 in the lab, before hand chlorination. Figure 35 shows results obtained by taking the same ozonated 1° filtrates, and then hand chlorinating the water without modifying the pH. Figure 36 shows the results from taking unozonated 1° filtrate, adjusting its pH in the lab to various pHs, and then hand chlorinating.

From figure 34, it can be seen that there was no effect of ozonation pH when the pH of the ozonated water was adjusted to 9, in the lab, before hand chlorination.

From figures 35 and 36, it can be seen that it was the hand chlorination pH (i.e. disinfection, or final water pH), that was important for THM production. Above a pH of about 7, THM formation was constant, but below a pH of about 7, THM formation dropped rapidly. This effect was true for both the unozonated, and the ozonated samples and is consistent with the fact that the THM formation reaction is favoured by alkaline conditions.

Figure 37 shows the results for AOX; although ozonation reduced AOX production, there was no consistent effect of pH.

3.3.6 Effect of Dual Point Ozonation

The effect of dual point ozonation on disinfection by-products is the same as combining the effects of ozonation at each point.

SECTION 4 - CONCLUSIONS AND RECOMMENDATIONS

- (i) When ozonating waters containing manganese, oxidised, colloidal manganese may be formed which cannot be removed by subsequent filtration. Site specific investigations into this effect are therefore necessary if ozone is to be used.
- (ii) Prechlorination increases disinfection by-products.
- (iii) Preozonation does not affect THM formation, but can reduce AOX and mutagenic activity.
- (iv) Small preozonation doses (up to 2 mg/l) may allow a small reduction in coagulant dose but large preozonation doses (greater than 4 mg/l) appear to disrupt the coagulation/flocculation process, resulting in poor quality final water.
- (v) If preoxidation is considered necessary (i.e. when there are algal problems) then ozone at low doses should be considered instead of chlorine to maintain low levels of disinfection by-products.
- (vi) Increasing interfiltration chlorine dose allows a reduction in the final disinfection chlorine dose but results in increased overall chlorine consumption and THMs.
- (vii) Continuous interfiltration chlorination may not be necessary for manganese removal if pH control is good. However, chlorination will compensate for the effects of poor pH control.
- (viii) Interfiltration or postozonation reduces disinfection by-products (but not chlorine consumption) and, for the quality of water encountered in this study, only a short ozone contact time is required.
- (ix) For AOX and THM reduction, only a small ozone dose is required (about $0.3 \, \text{mg/l}$) but for uv absorbance and mutagenic activity reduction, the optimum ozone dose is greater (about $2 \, \text{mg/l}$).

SECTION 5 - REFERENCES

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SECTION 6 - ACKNOWLEDGEMENT

The authors would like to thank the supply staff of North West Water, Eastern Division for their willingness to help whenever asked.

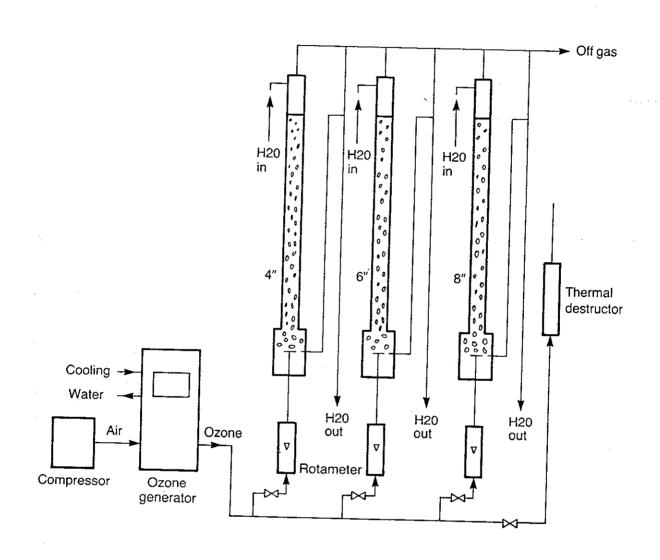


Figure 1 Ozone Flowsheet

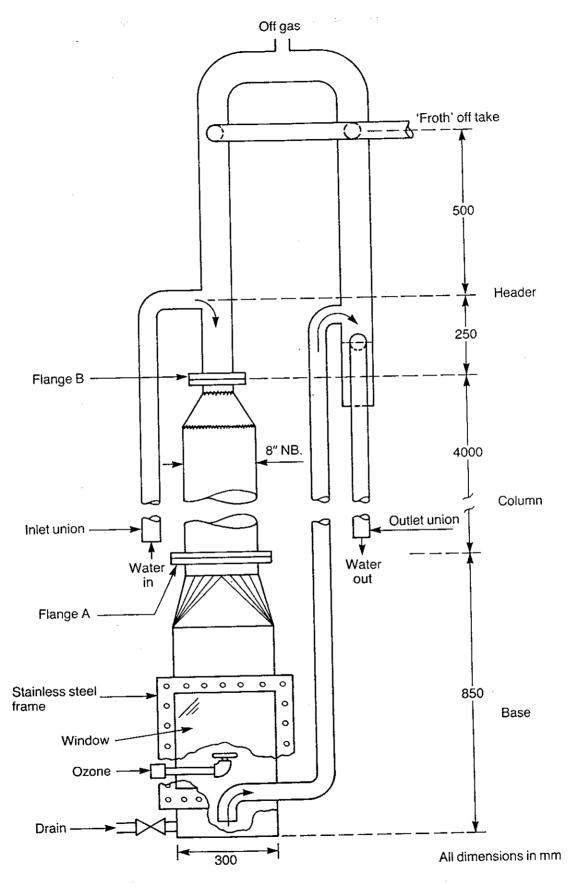


Figure 2 8" NB. Ozone Contactor

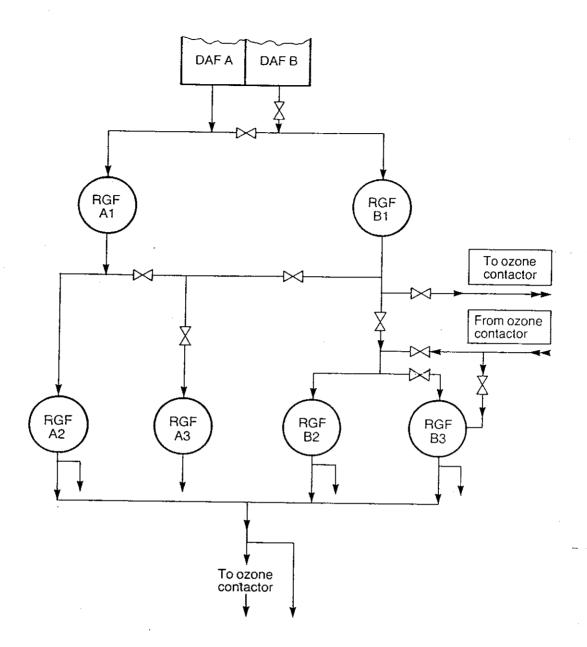


Figure 3 Flowsheet Showing Modified Pipework for Phase 2

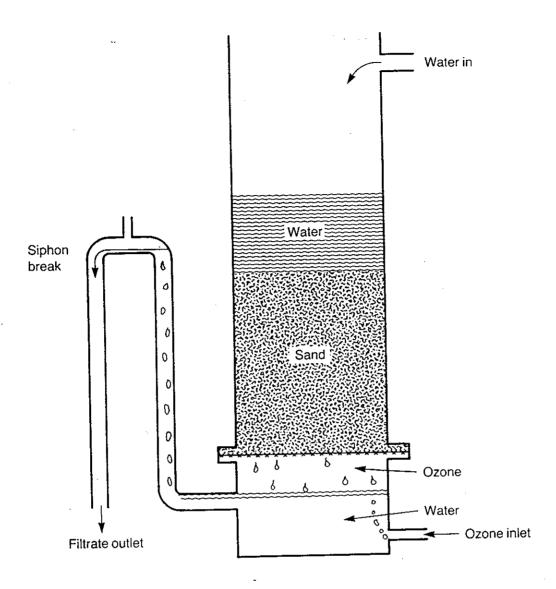
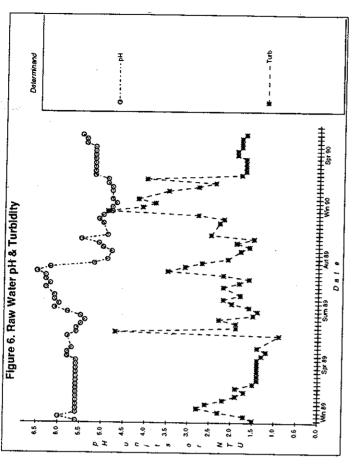
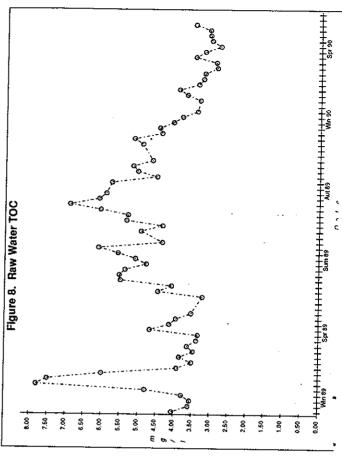
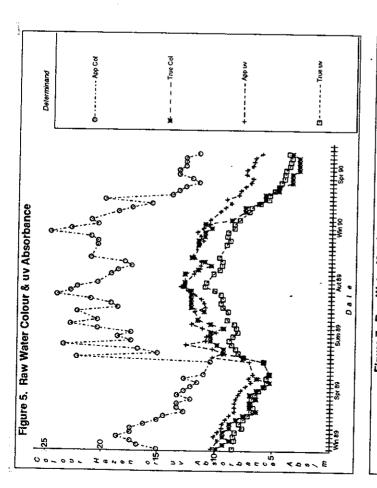
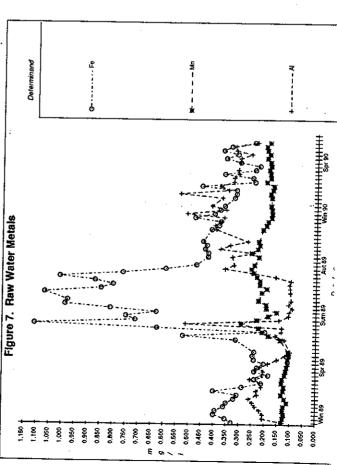


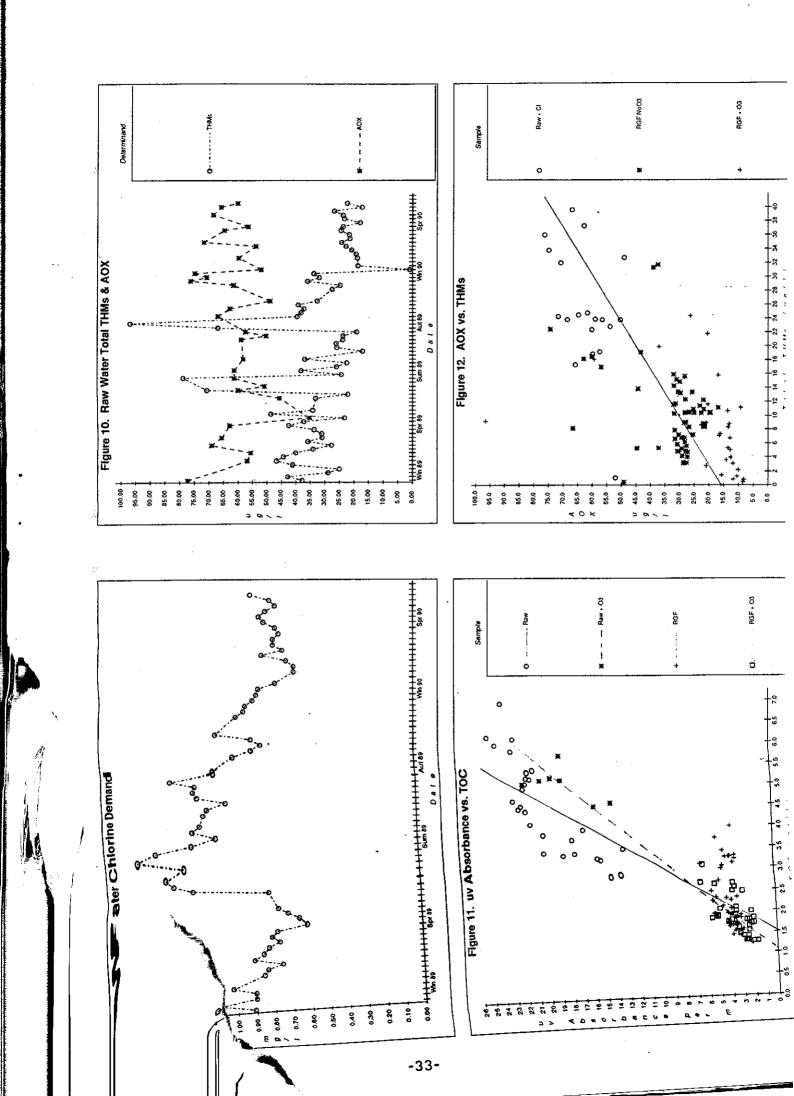
Figure 4 Application of Ozone During "Direct Ozonation" of an RGF

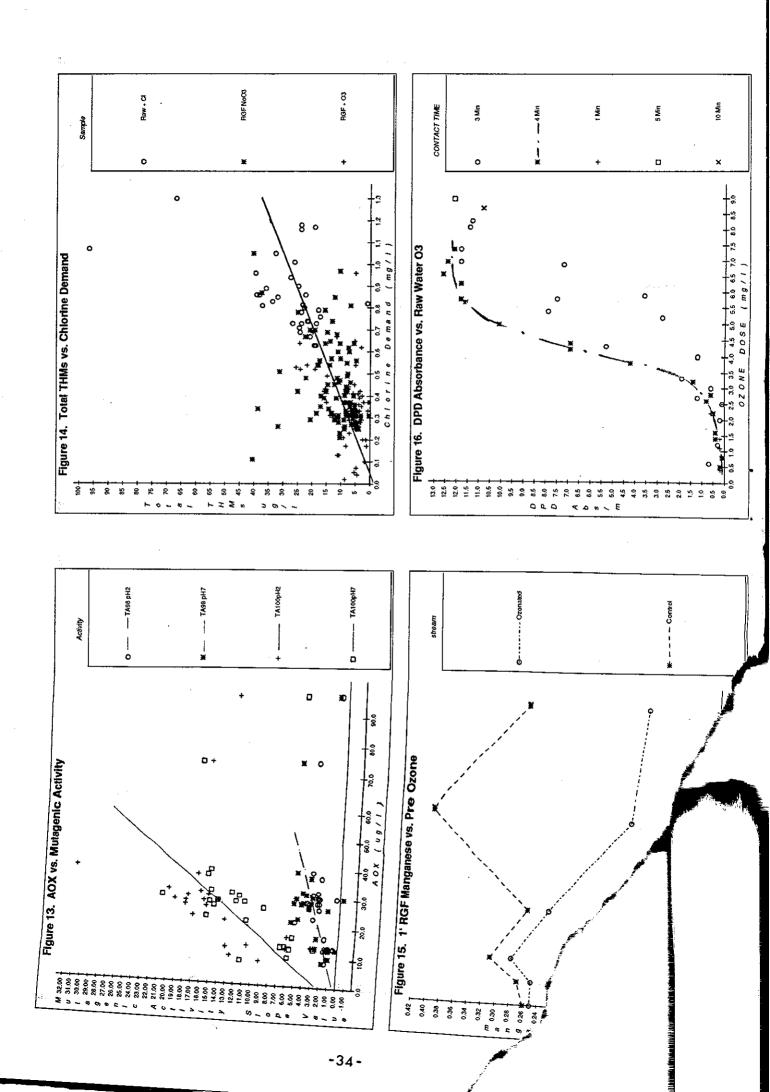


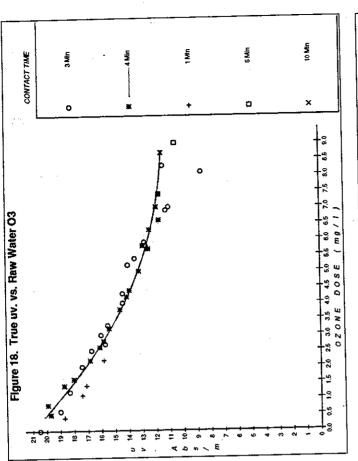


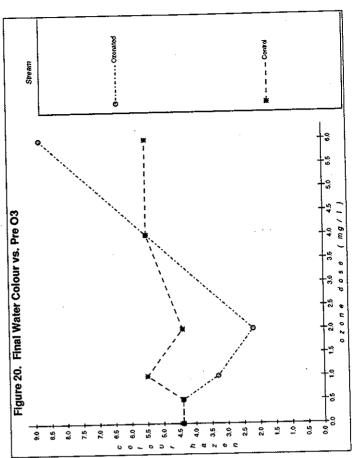


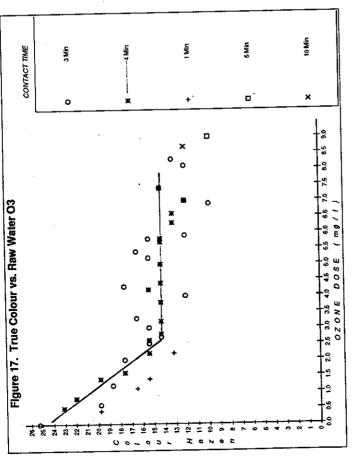


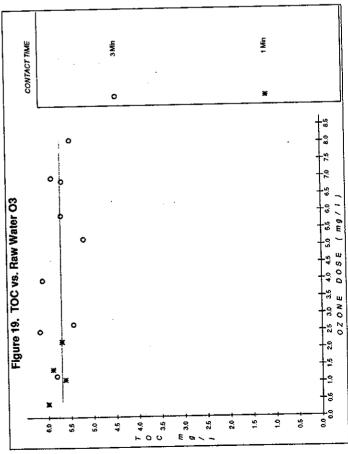


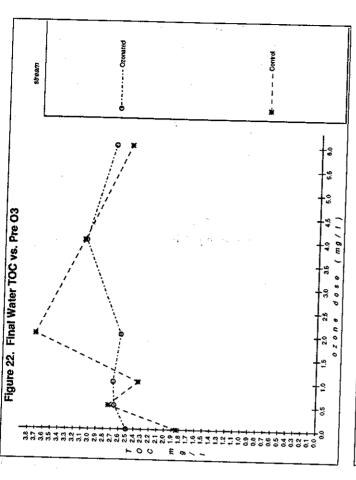


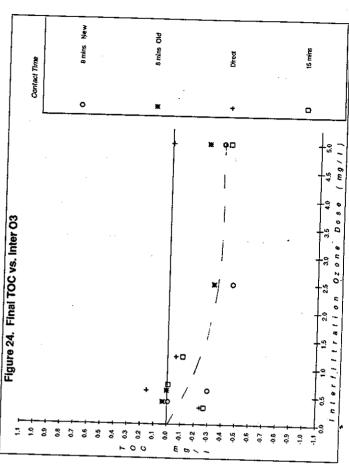


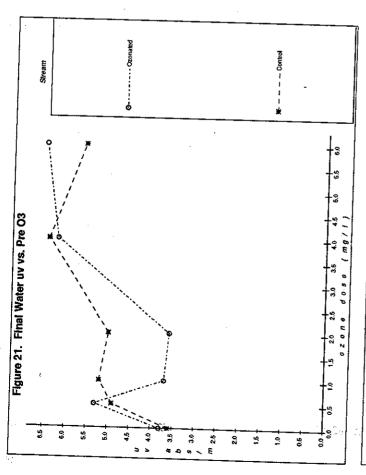


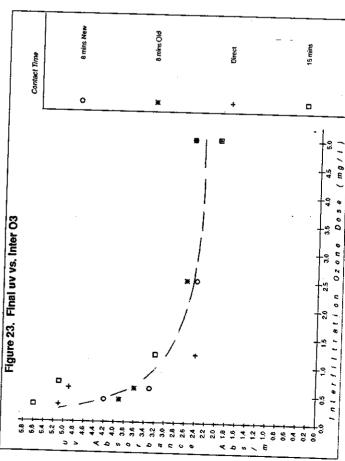


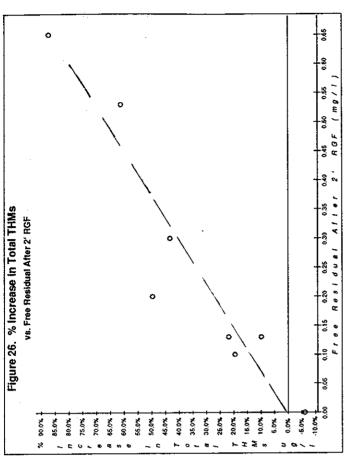


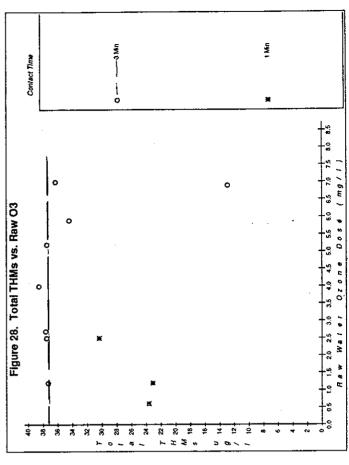


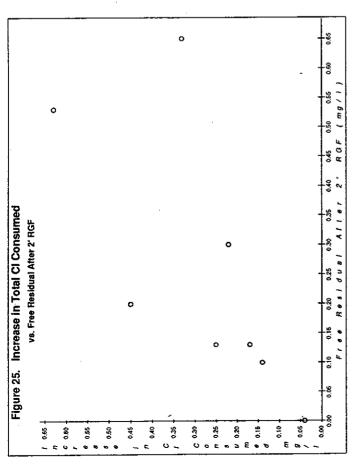


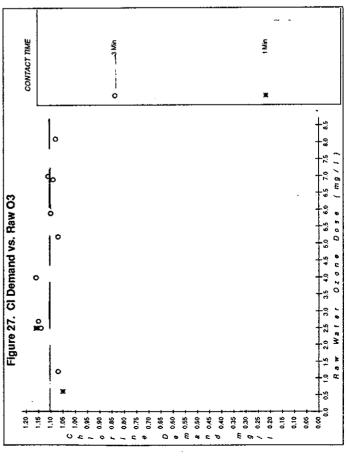


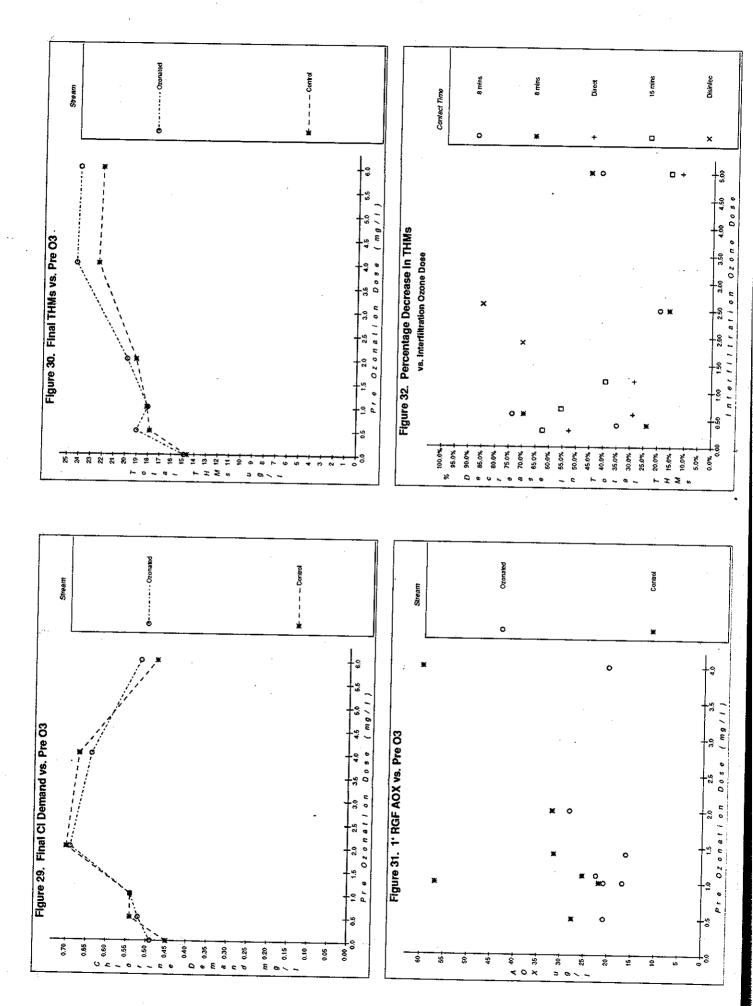


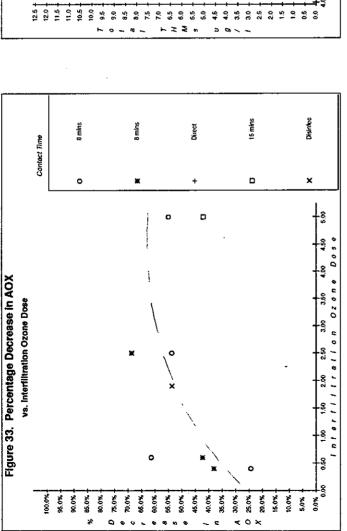


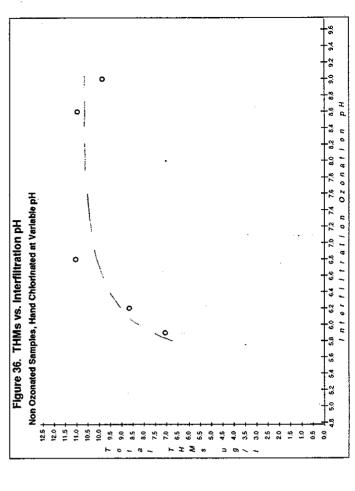


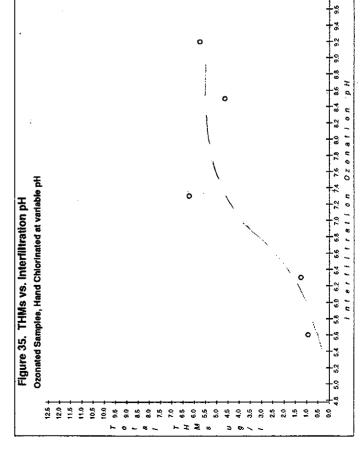












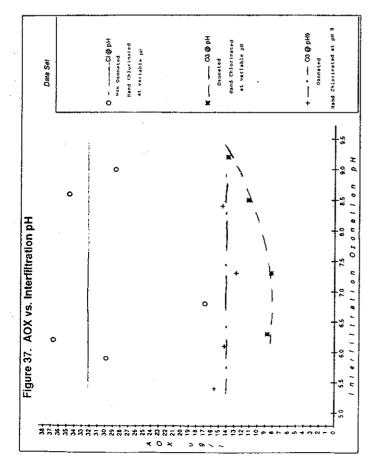
8.8 9.0 9.2 9.4 9.6

5,0 5,2 5,4 5,6 5,8 6,0 6,2

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Ozonated Samples, Hand Chlorinated at pH 9

Figure 34. THMs vs. Interfiltration pH



APPENDIX A - OZONE CONTACTORS DETAILED DESCRIPTION

Figure 2 shows a drawing of the 8" contactor. The contactor can be divided into three sections; the base section below flange A, the top section above flange B, and the middle section between the two flanges. Each of the three contactors is constructed from identical base and top sections, with a different bore middle section.

The base section is 300mm square in cross section, and 850mm from the bottom to flange A, which is 8" nominal bore. One side of the square section contains a clear 'Lexan' viewing window, held in place by a stainless steel frame. The ozone inlet is made from ½" N.B. stainless steel, and ends in a diffuser made from sintered steel. The water outlet is made from 1½" N.B. stainless steel, and is taken from the bottom of the contactor up to the top of the column, and then down to a 1½" union. This arrangement prevents the column from draining if the feed flow stops.

The middle section of the contactor consists of a 4m section of 8" N.B. stainless steel pipe, ending in flange A at one end and flange B at the other. For the other contactors, the middle section consists of a 4m section of 6" N.B. or 4" N.B. stainless steel pipe, ending in the same size flanges.

The top section of the column starts at flange B, which is 3" N.B. The feed enters 250mm above flange B (in 1½" N.B. stainless steel ending in a union), and there is an overflow take off 750mm above flange B. Above the overflow take off, the top section forms a U-bend, with the off gas outlet at the top of the bend. The other side of the U-bend (also connected to the overflow take off) collects water from the water outlet, and feeds this to the outlet union. This arrangement prevents syphoning of the contents of the contactor.

Table A1 shows the volumes of the three contactors. For each contactor, two values are given. The first is the volume of water above the diffuser, assuming that this is equal to a column 4.85m tall at the relevant diameter; the second is the volume of the base section (60 1) plus the volume of the 4m tall column, at the relevant diameter, above the box. The "nominal contact" time is based on the second volume.

Table A1 - Ozone Contactor Volumes (all values rounded to nearest 51)

Contactor	Volume of 4.85m Section of Column	Total Volume Including Base Section
Small	40	90
Medium	85	130
Large	150	185

APPENDIX B - TABLES OF RESULTS

All of the analytical results are provided in this appendix in the following tables:

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Trial 1	Pre and interfiltration chlorination	B1.1 to B1.17
Trial 2a	Raw water ozonation	B2a.1 to B2a.5
Trial 2b	Effect of preozonation	B2b.1 to B2b.17
Trial 3a	Effect of interfiltration czonation:dose	B3a.1 to B3a.19
Trial 3b	Effect of interfiltration ozonation:pH	B3b.1 to B3b.19
Trial 3bR	Effect of interfiltration ozonation:pH and	
	hand chlorination pH	B3bR.1 to B3bR.4
Trial 3c	Effect of ozone disinfection (postozonation)	B3c.1 to B3c.7
Trial 4	Effect of dual point ozonation	B4.1 to B4.18

Unless indicated otherwise, values in brackets in the tables refer to the control stream.

PHASE II. TRIAL 1. EFFECT OF PRE AND INTER FILTRATION CHLORINATION

This trial consisted of six runs, of which two investigated pre-chlorination, and the remaining four investigated inter-filtration chlorination. In the tables below, all the results are presented together. The first two rows in each table are the results for prechlorination, and the last four rows in each table are the results for inter-filtration chlorination.

PILOT PLANT CONTROL

For three of the runs during this trial, the final pHs were high (up to 9.4) on the morning of sampling. When this occurred, the final caustic dose was reduced, and the final water sampled later in the day. If the pH was still too high, it was reduced in the lab for hand chlorination.

Table B1.1 - Coagulant Doses and Sample pHs

יות ג כו	DOCE (ma Eo/l)	рН			
DATE	DOSE (mg Fe/l)	RAW WATER	DAF TREATED	1° RGF	2° RGF
3 Oct 89 10 Oct 89 17 Oct 89 24 Oct 89 31 Oct 89 7 Nov 89	4.3 4.5	6.3 6.5 6.2 5.2 4.9	4.6 (4.6) 4.6 (4.6) 4.6 4.7 4.6 4.7	6.6 (6.5) 6.4 (6.5) 6.6 6.7 6.5 6.4	9.1 (9.2) 8.7 (8.7) 9.1 (8.9) 9.4 (9.2) 9.1 (9.1) 9.0 (9.1)

Table Bl.1a - Trial Stream Prechlorination Dose

	DOSE	DAF O	VERFLOW	1° RG	F
DATE	(mg/l)	FREE	TOTAL	FREE	TOTAL
3 Oct 89 10 Oct 89	1.76 1.30	0.35 0.19	0.36		0.11

Table B1.2 - Colour: °Hazen (= Abs/m @400nm * 11)

	PRE			ST Cl	RAW !	WATER	DAF FI	LOATED	1°	2°
	DOS (mg/			SIDUAL ng/1)	APP	TRUE	APPARENT	TRUE	RGF	RGF
- 1	1.76 1.30 0 0 0	(0) (0) (0) (0) (0) (0)	0.18 0.08 0.00 0.30 0.53 0.65	(0.10) (0.06) (0.13) (0.10) (0.20) (0.13)	36 40 45 42 39 43	23 23 23 24 24 24 23	13 (15) 15 (18) 20 18 15	2 (2) 2 (2) 3 4 3 3	2 (2) 2 (2) 4 3 3	3 (3) 2 (2) 6 (4) 3 (4) 3 (3) 2 (3)

Table B1.3 - u.v. Absorbance (Abs/m @ 254nm)

	E Cl OSE		ST Cl SIDUAL	RAW	WATER	DAF FLO	OATED	1°	2°
	ig/l)	1	ng/l)	APP	TRUE	APPARENT	TRUE	RGF	RGF
1.7 1.3 0 0 0	0 (0) (0) (0)	0.53	(0.20)	22.5 24.8 24.1	17.8 18.1 20.8 20.6	7.9 (8.8) 8.8 (9.5) 10.3 12.2 10.9 10.6	3.2 (3.3) 3.2 (3.4) 3.6 5.1 5.1 4.5	3.5 (3.6) 3.4 (3.5) 3.8 4.4 4.6 4.5	3.4 (3.7) 3.4 (3.6) 3.9 (3.8) 4.3 (4.6) 4.5 (4.6) 4.2 (4.4)

Table B1.4 - Turbidity (NTU)

PRE C1 DOSE	POST C1 RESIDUAL	RAW	DAF	1°	2°
(mg/l)	(mg/l)	WATER	FLOATED	RGF	RGF
1.76 (0) 1.30 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	1.6 2.2 3.5 2.7 2.1 3.1	0.7 (0.8) 1.0 (1.0) 1.3 1.0 0.8 1.0	0.0 (0.0) 0.0 (0.0) 0.0 0.1 0.1 0.0	0.1 (0.1) 0.0 (0.0) 0.0 (0.0) 0.0 (0.1) 0.1 (0.1) 0.1 (0.1)

Table B1.5 - Total Organic Carbon (mg/l)

PRE (DOSE (mg/]	3	RES	ST Cl SIDUAL ng/l)	RAW WATER	FINAL WATER
1.30 (0 (0 (0 ((0) (0) (0) (0) (0)	0.18 0.08 0.00 0.30 0.53 0.65	(0.10) (0.06) (0.13) (0.10) (0.20) (0.13)	5.35 5.31 6.06 6.10 5.91 6.91	3.21 (3.98) 3.29 (3.11) 3.26 (3.27) 2.33 (2.14) 3.04 (2.99) 3.25 (3.41)

Table B1.6 - Iron (mg/l)

1	PRE Cl POST Cl DOSE RESIDUAL		RAW	DAF	1°	2°	
(mg/			ng/l)	WATER	FLOATED	RGF	RGF
1.76 1.30 0 0 0	(0) (0)	0.18 0.08 0.00 0.30 0.53 0.65	(0.10) (0.06) (0.13) (0.10) (0.20) (0.13)	0.80 0.87 1.01 0.59 0.47 0.76	0.71 (0.96) 0.82 (0.99) 1.10 1.00 0.79 0.98	0.04 (0.02) 0.03 (0.02) 0.03 0.04 0.03 0.03	0.02 (0.03) 0.02 (0.03) 0.02 (0.02) 0.04 (0.04) 0.02 (0.02) 0.01 (0.00)

Table B1.7 - Manganese (mg/l)

PRE C1	PRE Cl POST Cl DOSE RESIDUAL		DAF	1°	2°
(mg/l)	(mg/l)	WATER	FLOATED	RGF	RGF
1.76 (0) 1.30 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	0.23 0.25 0.24	0.20 (0.20) 0.21 (0.22) 0.23 0.25 0.26 0.24	0.21 (0.21) 0.21 (0.22) 0.23 0.26 0.26 0.30	0.00 (0.00) 0.00 (0.00) 0.00 (0.00) 0.00 (0.00) 0.00 (0.01) 0.01 (0.02)

Table B1.8 - Aluminium (mg/l)

PRE C1	POST C1	RAW	DAF	1°	2°
DOSE (mg/l)	RESIDUAL (mg/l)	WATER	FLOATED	RGF	RGF
1.76 (0) 1.30 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	0.10 0.10 0.16 0.36 0.32 0.25	0.04 (0.04) 0.02 (0.03) 0.05 0.21 0.24 0.12	0.03 (0.03) 0.01 (0.00) 0.01 0.03 0.02 0.01	0.03 (0.03) 0.00 (0.00) 0.00 (0.00) 0.02 (0.02) 0.02 (0.02) 0.01 (0.01)

Table B1.9 - Hand chlorinated final water - bacteriological quality

PRE C1 DOSE	POST C1 RESIDUAL	COLIFORMS *		CFU		
(mg/l)	(mg/l)	E-Coli	Total	37°C 1-Day	22°C 3-Day	
1.76 (0) 1.30 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	0 (0) 0 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0 (0) 0 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0 (0) 0 (0) 0 (0) 1 (1) 0 (0) 0 (0)	0 (0) 0 (0) 6 (0) 0 (11) 0 (0) 1 (0)	

 * per 100 ml CFU : colony forming unit per ml

Table B1.10 - Chloroform (ug/l)

PRE C		POST C1 RESIDUAL	NON	DAND CETANI	HAI	ND CHLOR:	INATED
(mg/l		(mg/l)	2°	RGF	RAW	1° RGF	2° RGF
1.30 (0 (0 (0 (0) 0. 0) 0. 0) 0.	0.06)	20.80 2.95 10.05 20.20	(8.36) (7.72) (5.63) (5.60) (15.22) (3.1)	24.38 21.74 21.50 64.88 94.35 18.8	33.26 (12.41) 25.29 (11.48) 9.19 16.62 22.95 5.3	31.49 (13.68) 24.97 (13.39) 8.47 (10.12) 24.08 (20.14) 37.35 (35.07) 9.7 (6.5)

Table B1.11 - Bromodichloromethane (ug/l)

PRE C1 DOSE	POST C1 RESIDUAL	NON HAND CHLORINATED	HAND CHLORINATED				
(mg/l)	(mg/l)	2° RGF	RAW	1° RGF	2° RGF		
1.30 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	5.01 (1.39) <0.01 (1.70) 0.46 (0.21)	1.73 1.97 2.21 1.38 2.28 0.3	6.38 (1.47) 5.55 (1.72) 1.85 0.71 1.80 0.2	6.33 (1.65) 5.47 (2.02) 1.89 (2.01) 0.80 (0.59) 2.76 (2.16) 0.6 (0.2)		

Table B1.12 - Dibromochloromethane (ug/l)

PRE C1	PRE C1 POST C1 DOSE RESIDUAL			NON	HAND INATED	HAND CHLORINATED			
(mg/l)			ig/l)	2°	RGF	RAW	1° RGF	2° RGF	
 0 (0 0 (0 0 (0))))))	0.08 0.00 0.30 0.53	(0.10) (0.06) (0.13) (0.10) (0.20) (0.13)	0.81 <0.05 <0.05 0.13	(<0.05) (0.12) (<0.05) (0.06) (0.14) (<0.1)	<0.05 0.14 <0.05 0.66 0.13 <0.1	0.81 (<0.05) 0.83 (0.12) <0.05 <0.05 0.12 <0.1	0.81 (0.15) 0.82 (0.16) <0.05 (<0.05) <0.05 (<0.05) 0.17 (0.17) <0.1 (<0.1)	

Table B1.13 - Bromoform (ug/l)

PRE Cl POST Cl DOSE RESIDUAL			NON	HAND	HAND CHLORINATED				ΕD	
(mg/					RGF	RAW	1° R	GF	2°	RGF
1.30 0 0	(0) (0) (0) (0)	0.08 0.00 0.30 0.53	(0.10) (0.06) (0.13) (0.10) (0.20) (0.13)	<0.03 <0.03 <0.03 <0.03	(<0.03) (<0.03) (<0.03) (<0.03) (<0.03) (<0.02)	<0.03 <0.03 <0.03 <0.03 <0.03	<0.03 (3 <0.03 (3 <0.00 <0.00 0.1 <0.0	<0.03) 3 3 4	<0.03 <0.03 <0.03 <0.03	(<0.03) (<0.03) (<0.03) (<0.03) (<0.03) (<0.2)

Table B1.14 - Total trihalomethanes (ug/l)

	Cl SE	POST Cl RESIDUAL	NON HAND CHLORINATED	H A I	ND CHLOR	INATED
l l	(/1)	(mg/l)	2° RGF	RAW	1° RGF	2° RGF
1.76 1.30 0 0 0	(0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	34.02 (9.70) 26.65 (9.26) 3.04 (7.41) 10.59 (5.90) 22.12 (16.90) 6.2 (3.1)	26.19 23.88 23.79 66.95 96.79 19.1	40.48 (13.96) 31.70 (13.35) 11.12 17.41 25.01 5.5	38.66 (15.51) 31.29 (15.60) 10.44 (12.21) 24.96 (20.81) 40.31 (37.43) 10.3 (6.7)

[#] These samples were analysed by WRc Medmenham.

Table B1.15 - Chlorine demand (mg/l)

PRE C1 DOSE	POST C1 RESIDUAL	RAW	1° RGF		2° RGF	
(mg/l)	(mg/l)	10211	1 1(61	FILTER	LAB	TOTAL
1.30 (0) 0 (0) 0 (0) 0 (0)	0.18 (0.10) 0.08 (0.06) 0.00 (0.13) 0.30 (0.10) 0.53 (0.20) 0.65 (0.13)	1.16 1.18 1.30 1.07	0.26 (0.57) 0.60 0.56 0.42	0.25 (0.54) 0.39 (0.65) 0.00 (0.74) 0.66 (0.55) 0.88 (0.78) 0.84 (0.70)	0.12 (0.14) 0.64 (0.11) 0.12 (0.15) 0.17 (0.09)	0.51 (0.79) 0.64 (0.85) 0.78 (0.70) 1.05 (0.87)

Table B.116 - Adsorbable organic halide (AOX) (ug/l)

PRE C1	POST C1	NON HAND	HAND CHLORINATED		
DOSE	RESIDUAL	CHLORINATED			
(mg/l)	(mg/l)	2° RGF	RAW	1° RGF	2° RGF
0 (0)	0.08 (0.06)	29.6 (16.0)	58.9	37.3 (25.7)	38.9 (28.2)
	0.00 (0.13)	<8 (12.3)	50.3	16.9	19.5 (21.9)
	0.65 (0.13)	24.3 (20.8)	57.4	27.6	25.0 (29.3)

Table B1.17 - Mutagenic activity (slope value)

PRE C1	NON CHLORINATED					HAND CHLORINATED FINAL WATER						· · ·
DOSE	T	RIAL	1° R	GF	ŗ	TRIAL STREAM		CONTROL		STREAM		
(mg/l)	TA	98	TA	100	TA	98	TA	100	TA	98	TA	100
	рН 2	рн 7	рН 2	рН 7	рН 2	рн 7	рН 2	рн 7	рН 2	рн 7	рН 2	рН 7
1.30 (0)	1.53	4.37	12.02	10.56	3.32	5.15	31.01	15.32	2.66	3.38	16.01	11.21

PHASE II. EXPERIMENT 2a). EFFECT OF RAW WATER OZONATION

Five trials were carried out, each at a different contact time, to investigate the effect of raw water ozonation. A summary of the conditions used for each trial is given in table B2a.1.

RESULTS

The raw water quality for each day of the trials is shown in table B2a.2.

Table B2a.3 shows the conditions recorded from the ozone generator and contactor during each run. The final column gives the ozone dose calculated from the previous columns. For each trial, the rows are in order of target ozone dose, which increased from 0.5 to 9.0 in 0.5 mg/l increments for trials A and B, and from 0.5 to 2.0 in increments of 0.5mg/l for trial C. The same order of rows is used in table B2a.4, which gives the onsite analyses for each run. Table B2a.5 gives the offsite TOC and THM analyses, as well as chlorine demand. A simplified hand chlorination procedure was used, where a constant chlorine dose (of 1.5 mg/l) was applied to each sample. Samples for offsite analyses covered ozone doses of 1 to 9 in increments of 1 mg/l.

Table B2a.1 - Summary of Trial Conditions

TRIAL	02	ONE	RAW WATER	CONATACT
	CONCENTRATION	FLOWRATE	FLOW (1/hr)	TIME (mins)
A	FIXED	VARIED	3600	3
В	VARIED	FIXED	2800	4
С	FIXED	VARIED	3600	1.5
D	SINGLE	RUN	2200	5
E	SINGLE	RUN	1100	10

Table B2a.2 - Raw Water Quality During Trials

DATE	рН	TURBIDITY	CO	LOUR	UV	UV		
		(NTU)	APPARENT (Abs/m)	TRUE (Abs/m)	APPARENT (Abs/m)	TRUE (Abs/m)		
8 Nov 89 9 Nov 89 10 Nov 89 13 Nov 89 15 Nov 89 16 Nov 89	4.9 4.8 4.7 4.9 4.7	2.1 2.1 2.0 2.0 1.9 1.8	3.6 3.7 3.5 3.4 3.4 3.3	2.4 2.2 2.2 2.1 2.1 2.0	23.9 24.0 23.9 23.7 23.7 23.2	20.6 20.5 20.4 20.2 20.1 19.8		

Table B2a.3 - Ozone generator and contactor conditions

TRIAL	DATE	TIME		GENER <i>I</i>	ATOR	CON.	PACTOR	OZON	E
			FLOW	POWER	PRESSURE	GAS FLOW	WATER FLOW	CONC	DOSE
			l/hr	(W)	(kPa)	(l/hr)	(1/hr)	g/m3	mg/l
A	10/11 09/11 10/11 09/11 10/11 09/11 08/11 09/11 08/11 09/11 08/11 09/11 08/11 09/11 08/11	09.20 09.15 10.25 09.55 09.45 14.25 13.20 12.20 11.30 13.40 15.25 11.55 14.45 10.40 12.20 13.00 16.00 15.05	1650 1700 1700 1700 1600 1700 1750 1750 1750 1750 1750 1600 1800 1600	140 140 140 140 400 400 400 420 400 400 420 400 400 4	690 700 740 710 700 730 720 710 690 730 720 730 690 750 740 720 720	350 680 1080 1370 1630 530 650 790 860 1040 1080 1180 1150 1370 1480 1400 1650	3600 3600 3600 3600 3600 3600 3600 3600	6.6 6.6 6.6 6.6 18.0 18.0 18.0 18.0 18.0 18.0 18.0 18.0	0.6 1.2 2.0 2.5 3.0 2.7 3.3 4.0 4.3 5.2 5.4 5.9 7.4 7.0 8.3 8.1
В	15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11 15/11	09.10 11.45 13.25 11.15 10.05	800 800 850 850 850 800 800 800	70 095 115 130 150 185 210 225 265 290 325 370 410 470	600 610 610 610 610 610 610 610 610 610	530 820 820 820 820 820 820 820 820 820 82	2800 2800 2800 2800 2800 2800 2800 2800	2.7 2.7 4.9 5.6 7.4 8.8 9.6 10.9 12.9 14.3 15.0 17.0 18.1 19.6 21.4 22.6 23.9 25.2	0.5 0.8 1.4 1.6 2.2 2.8 3.2 3.8 4.2 4.4 5.8 5.7 6.6 7.0 7.4
С	13/11 13/11 13/11 13/11	13.35	400	190	670 650 620 640	41 138 186 284	3600 3600 3600 3600	28 28 28 28	0.4 1.1 1.4 2.2
D	16/11		1200	310	670	1100	2200	18	9.0
E	16/11		600	150	500	530	1100	18	8.7

Table B2a.4 - Onsite analyses for each run

						1 Caci	1011	
CONTA		E TURBIDIT	Y pH	DPD	CO	LOUR	UV ABSO	RBANCE
TIME (mins		l) (NTU)		(Abs/m)	APPARE (Abs/m		APPAREN (Abs/m)	T TRUE Abs/m
*3	0.6 1.2 2.0 2.5 3.0 2.7 3.3 4.0 4.3 5.2 5.4 5.9 5.8 6.9 7.0 8.3 8.1	1.9 1.9 2.0 1.8 1.9 1.8 1.7 1.7 1.7 2.0 2.6 2.6 2.6 3.9	4.7 4.7 4.7 4.7 4.7 4.6 4.5 4.6 4.6 4.5 4.5 4.5 4.5	0.3 0.2 0.1 0.6 1.2 1.9 1.2 5.3 2.8 7.9 3.6 7.5 7.2 11.8	3.2 3.0 2.8 2.6 2.6 2.4 2.5 2.1 2.6 2.4 2.5 2.7 2.5 2.7 2.5 2.6 2.8	1.8 1.7 1.6 1.4 1.3 1.5 1.1 1.6 1.4 0.9 1.3 1.1	21.6 20.7 19.8 19.1 18.8 18.5 17.3 17.0	19.0 18.3 17.4 16.7 16.0 15.7 15.5 14.4 14.0 13.5 12.8 12.7 11.2 11.7 11.0 11.4 8.6
4	0.5 0.8 1.4 1.6 2.2 2.6 2.8 3.2 3.8 4.2 4.4 5.0 5.8 5.7 6.3 6.6 7.0 7.4	1.9 1.8 1.8 1.8 1.8 1.7 1.7 1.7 1.7 1.7 1.7 1.6 1.6 1.7 1.7	NA N	0.2 0.1 0.4 0.5 0.8 0.6 1.4 4.2 -6.9 6.9 10.1 11.8 11.6 11.8 12.6 12.4 12.1	3.4 3.3 3.1 2.8 2.6 2.5 2.4 2.3 2.4 2.3 2.3 2.2 2.3 2.1 2.1 2.1 2.0	2.1 2.0 1.8 1.6 1.4 1.3 1.3 1.3 1.3 1.3 1.3 1.3 1.3	23.3 23.3 22.2 21.3 19.9 19.2 18.8 18.3 17.4 16.9 16.7 15.7 15.5 15.0 14.7 13.8 14.1	19.7 19.9 18.7 18.0 16.8 16.1 15.8 14.6 14.1 13.9 13.2 12.9 12.5 12.4 11.7 11.9 11.7
1.5	0.4 1.1 1.4 2.2	2.0 1.9 1.9 1.8	4.8 4.8 4.8 4.7	0.2 0.2 0.2 0.6	3.0 2.8 2.5 2.2	1.8 1.5 1.4 1.2	22.2 20.8 20.3 18.5	18.7 17.4 17.1 15.8
5	9.0	1.9	4.5	12.1	1.9	0.9	12.9	10.5
10	8.7	2.4	4.4	10.8	2.5	1.1	14.1	11.5

Table B2a.5 - Offsite analyses for each run

CONTACT	OZONE	TOC	HANI	HAND CHLORINATION				тнм	S	
TIME (mins)	DOSE (mg/l)	(mg/l)		DEMAND (mg/l)	RESIDUAL (mg/l)	C13 ug/l	Cl2Br ug/l	ClBr2 ug/l		Total ug/l
3	1.2 2.5 2.7 4.0 5.2 5.9 6.9 7.0 8.1	5.81 6.17 5.43 6.10 5.19 5.68 5.66 5.88 5.47	8.8 9.0 8.9 8.8 8.9 9.0 8.7 8.9	1.07 1.14 1.15 1.16 1.07 1.10 1.09 1.11	0.43 0.36 0.35 0.34 0.43 0.40 0.41 0.39 0.42	35.33 35.55 35.61 36.43 35.40 32.28 11.27 33.97	1.72 1.77 1.83 1.94 1.89 1.96 1.39 2.12	0.18 0.17 0.19 0.17 0.17 0.16 0.17	0.09 <.03 <.03 <.03 <.03 <.03 <.03	
1.5	0.4 1.1 1.4 2.2	6.00 5.62 5.89 5.69	9.3 8.8 9.1 8.9	1.05 1.31 1.16	0.45 0.62 0.34	23.29 22.63 38.47 29.93	0.28 0.40 0.54 0.38	<.05 <.05 <.05 <.05	<.03 <.03 <.03 <.03	23.65 23.11 39.09 30.39

PHASE II. TRIAL 2b. EFFECT OF PREOZONATION

This trial included 7 runs where the ozone dose applied to the raw water was varied, prior to coagulation.

The ozone doses selected were 0.5, 1, 2, 4 and 6 mg/l. The two higher doses were used at a nominal 5 minute contact time, with the three lower doses at a nominal 1 minute contact time. After the completion of these five runs, two additional runs were made. The first additional run was a control run to investigate the effects of aeration prior to coagulation. A trial stream pre-ozonation dose of 0.0 mg/l was used for this run. The water was however contacted with air at the same air/water flowrates as the 6mg/l ozone dose run. For the final run, the possibility of reducing coagulant dose with pre-ozonation was investigated. For this run, a pre-ozonation dose of lmg/l was applied to the trial stream, and the trial stream ferric dose was reduced to give the same final water quality as the control stream.

PILOT PLANT CONTROL

Pilot plant control was generally good during this trial. There was one run with a low final pH (8.6) which was increased in the lab for hand chlorination. There was also one run with a low trial stream DAF pH (4.3).

Table B2b.1 - Doses and pHs

	FERRIC OZO		IE	рн					
DATE	DOSE (mg/l)	DOSE T	TIME	RAW	DAF FLOATED	1° RGF	2° RGF		
21 Nov 89 28 Nov 89 5 Dec 89 12 Dec 89 19 Dec 89 9 Jan 90 16 Jan 90	2.9 (3.3) 3.5 (3.3) 5.4 (5.5) 5.3 (5.5)	2 0.5 4 6 1 0.0	1 5 5 1 5	4.8 5.0 5.1 5.5 4.9 5.0 5.1	4.6 (4.6) 4.7 (4.6) 4.7 (4.6) 4.6 (4.6) 4.3 (4.6) 4.7 (4.6) 4.6 (4.6)	6.6 (6.6) 6.5 (6.5) 6.5 (6.5) 6.5 (6.5) 6.3 (6.6) 6.6 (6.6) 6.4 (6.5)	8.9 (8.9) 8.6 (9.0) 8.8 (9.1) 8.9 (9.0) 8.8 (9.0) 9.1 (9.0) 8.9 (8.9)		

Table B2b.2 - Colour: °Hazen (= Abs/m @400mm * 11)

OZONE	RAW V	WATER	OZONI	E RAW		DAF FLO	ATEC)	1°	RGF	2°	RGF
DOSE (mg/l)	APP	TRUE	APP	TRUE	APF	ARENT	TF	RUE				
0.0 0.5 1 2 4 6 Low Fe	38 35 40 36 33 34 39	22 22 23 24 20 21 22	38 31 32 26 19 30 33	21 18 17 14 11 12 17	14 17 18 18 15 23 17	(20) (20) (17) (21) (15) (20) (18)	3 4 3 2 4 4	(3) (4) (3) (4) (3) (4) (4)	3 4 2 2 6 9 3	(3) (4) (4) (3) (4) (6) (4)	4 4 3 2 6 9 4	(4) (4) (6) (4) (6) (6) (4)

Table B2b.3 - U.V. (Abs/m @ 254nm)

OZONE	RAW W	VATER	OZONE	E RAW	DAF FLOATED			10	RGF	2°	RGF	
DOSE (mg/l)	APP	TRUE	APP	TRUE	APP	ARENT	TF	UE				
0.0 0.5 1 2 4 6 Low Fe	22.0 22.7 22.7 21.6 21.5	18.4 18.5 19.4 18.0 17.9	20.3 19.4 18.5 15.6 14.1	16.9 15.4 15.5 12.6 11.0	11.0 10.2 11.3 10.6 12.6	(10.4) (12.0) (9.8) (12.8) (10.8) (11.3) (9.5)	4.6 4.0 4.5 4.4 4.8	(5.0) (3.8) (5.3) (4.5)	3.3 3.7 5.7 6.6	(5.1) (5.2) (5.9)	3.8 5.3 3.7 3.6 6.2 6.5 2.9	(3.6) (4.9) (5.2) (5.0) (6.4) (5.6) (3.4)

Table B2b.4 - Turbidity (NTU)

OZONE DOSE	RAW WATER		DAF	1.0	DOD		
(mg/l)	APP	OZONE	FLOATED	l 1°	RGF	2°	RGF
0.0 0.5 1 2 4 6 Low Fe	2.3 1.6 2.5 1.8 1.9 1.5 2.2	2.3 1.6 2.3 N/A 1.3 2.1 2.3	0.7 (0.8) 1.0 (1.0) 0.9 (0.7) 0.9 (1.0) 1.0 (0.9) 1.5 (1.0) 1.0 (1.1)	0.1 0.1	(0.1) (0.1) (0.1) (0.1) (0.1) (0.1) (0.1)	0.1 0.1 0.0 0.2	(0.1) (0.0) (0.1) (0.0) (0.1) (0.1) (0.1)

Table B2b.5 - TOC (mg/l)

OZONE DOSE	RAW	WATER	FINAL		
(mg/l)	NO 03	OZONE	WATER		
0.0 0.5 1 2 4 6 Low Fe	4.93 4.52 4.65 5.76 5.05 5.18 5.16	5.05 5.13 5.18 5.13 4.49 4.57 5.66	2.50 (1.84) 2.66 (2.74) 2.68 (2.35) 2.59 (3.71) 3.07 (3.09) 2.71 (2.50) 2.49 (2.35)		

Table B2b.6 - Iron (mg/l)

OZONE DOSE (mg/l)	RAW WATER	DAF FLOATED	1° RGF	2° RGF
0.0	0.41	1.29 (1.19)	0.03 (0.03)	0.01 (0.01)
0.5	0.43	1.06 (0.96)	0.05 (0.02)	0.07 (0.03)
1	0.45	1.37 (0.99)	0.08 (0.09)	0.04 (0.07)
2	0.43	1.21 (0.90)	0.03 (0.03)	0.02 (0.02)
4	0.44	1.23 (0.93)	0.28 (0.07)	0.30 (0.09)
6	0.43	1.78 (1.04)	0.52 (0.11)	0.44 (0.07)
Low Fe	0.38	0.93 (1.58)	0.05 (0.03)	0.02 (0.01)

Table B2b.7 - Manganese (mg/l)

OZONE DOSE (mg/1)	RAW WATER	DAF FLOATED	1° RGF	2° RGF
0.0	0.21	0.23 (0.24)	0.25 (0.26)	0.00 (0.00)
0.5	0.25	0.25 (0.27)	0.25 (0.27)	0.00 (0.00)
1	0.23	0.26 (0.27)	0.28 (0.31)	0.02 (0.00)
2	0.23	0.22 (0.25)	0.23 (0.26)	0.01 (0.00)
4	0.23	0.15 (0.26)	0.12 (0.40)	0.01 (0.01)
6	0.22	0.14 (0.25)	0.10 (0.27)	0.02 (0.00)
Low Fe	0.20	0.22 (0.23)	0.21 (0.22)	0.01 (0.00)

Table B2b.8 - Aluminium (mg/l)

OZONE DOSE (mg/l)	RAW WATER	DAF FLOATED	1° RGF	2° RGF
0.0	0.40	0.29 (0.25)	0.02 (0.02)	0.03 (0.04)
0.5	0.25	0.21 (0.21)	0.02 (0.02)	0.03 (0.03)
1	0.27	0.22 (0.20)	0.04 (0.05)	0.04 (0.07)
2	0.33	0.23 (0.23)	0.01 (0.02)	0.03 (0.06)
4	0.38	0.29 (0.24)	0.05 (0.07)	0.10 (0.17)
6	0.34	0.26 (0.19)	0.07 (0.04)	0.10 (0.05)
Low Fe	0.40	0.30 (0.32)	0.02 (0.03)	0.02 (0.02)

Table B2b.9 - Hand chlorinated final water bacteriological quality

OZONE DOSE	COLI	FORMS *	CFU			
(mg/l)	E-Coli	Total	1-Day	3 - Day		
0.0 0.5 1 2 4 6 Low Fe	0 (0) 0 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0 (0) 0 (0) 0 (0) 0 (0) 0 (0) 0 (0) 0 (0)	0 (0) 0 (0) 0 (0) 1 (3) 1 (0) 0 (0) 0 (0)	0 (0) 0 (2) 0 (0) 0 (0) 0 (0) 0 (0) 6 (3)		

 $\ensuremath{^{\star}}$ per 100 ml CFU : colony forming unit per ml

Table B2b.9b - Ozonated raw water bacteriological quality

OZONE DOSE	COL	IFORMS *	CF	U
(mg/l):	E-Coli	Total	37°C 1-Day	22°C 3-Day
0.0 0.5 1 2 4 6 Low Fe	3 1 0 0 0 0	6 0 8 0 0 0	10 100 1 4 24 0 2	488 0 68 62 0 2 712

* per 100 ml
CFU : colony forming units per ml

Table B2b.10 - Chloroform (ug/1)

OZONE DOSE	NON HAND CHLORINATED	НА	HAND CHLORINATED				
(mg/l)	2° RGF	RAW	1° RGF	2° RGF			
0.0 0.5 1 2 4 6 Low Fe	10.20 (8.47) 8.77 (7.70) 10.76 (10.84) 8.91 (N/A) 12.51 (12.62) 14.22 (12.56) 4.60 (4.22)	25.72 36.85 31.00 37.94 34.95 36.57 23.60	11.79 (10.92) 13.89 (15.88) 14.20 (15.36) 14.28 (14.68) 19.22 (16.36) 19.79 (18.42) 7.91 (7.53)	13.28 (13.00) 17.83 (16.57) 16.25 (16.46) 18.50 (18.04) 21.38 (19.91) 21.63 (19.81) 10.70 (9.42)			

Table B2b.11 - Bromodichloromethane (ug/1)

OZONE DOSE	NON HAND CHLORINATED	н А	HAND CHLORINATED							
(mg/l)	2° RGF	RAW	1° RGF	2° RGF						
0.0 0.5 1 2 4 6 Low Fe	1.55 (1.34) 0.80 (0.82) 1.31 (1.30) 0.81 (N/A) 1.87 (1.85) 1.88 (1.90) 0.52 (0.53)	1.69 1.31 1.64 1.51 2.23 2.44 0.78	1.53 (1.50) 1.06 (1.13) 1.48 (1.49) 1.05 (1.05) 2.15 (2.02) 5.45 (1.98) 0.71 (0.65)	1.53 (1.55) 1.12 (1.22) 1.64 (1.53) 1.24 (0.95) 2.53 (2.14) 2.29 (2.14) 0.72 (0.70)						

Table B2b.12 - Dibromochloromethane (ug/l)

OZONE DOSE	NON HAND CHLORINATED	на	ND CHLOR	INATED
(mg/l)	2° RGF	RAW	1° RGF	2° RGF
0.0 0.5 1 2 4 6 Low Fe	0.17 (<0.05) <0.05 (<0.05) <0.05 (<0.05) <0.05 (N/A) <0.05 (<0.05) 0.19 (0.22) <0.05 (<0.05)	<0.05 <0.05 0.11 <0.05 0.16	0.40 (<0.05) <0.05 (<0.05) <0.05 (<0.05) 0.09 (0.12) 0.37 (<0.05) 0.29 (0.16) <0.05 (<0.05)	<pre><0.05 (<0.05) <0.05 (<0.05) 0.13 (0.11) 0.11 (0.09) 0.41 (0.36) 0.16 (0.18) <0.05 (<0.05)</pre>

Table B2b.13 - Bromoform (ug/1)

OZONE DOSE	NON HAND CHLORINATED	нан	ND CHLOR:	INATED		
(mg/l)	2° RGF	RAW	1° RGF	2° RGF		
0.0 0.5 1 2 4 6 Low Fe	<pre><0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03) <0.03 (N/A) <0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03)</pre>	<0.03 <0.03 <0.03 <0.03 <0.03 <0.03	<pre><0.03 (<0.03) <0.03 (<0.03)</pre>	<0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03) <0.03 (<0.03) 0.13 (0.10)		

Table B2b.14 - Total trihalomethanes (ug/l)

OZONE DOSE	NON HAND CHLORINATED	HAI	HAND CHLORINATED								
(mg/l)	2° RGF	RAW	1° RGF	2° RGF							
0.0 0.5 1 2 4 6 Low Fe	11.95 (9.89) 9.65 (8.60) 12.15 (12.22) 9.80 (N/A) 14.46 (14.55) 16.32 (14.71) 5.20 (4.83)	39.59 37.26	13.75 (12.50) 15.03 (17.09) 15.76 (16.93) 15.45 (15.88) 21.77 (18.46) 25.56 (20.59) 8.90 (8.38)	14.89 (14.63) 19.03 (17.87) 18.05 (18.13) 19.88 (19.11) 24.35 (22.44) 24.11 (22.16) 11.60 (10.27)							

Table B2b.15 - Chlorine demand (mg/l)

OZONE DOSE	POST C1 RESIDUAL	RAW	10 PCF	2° RGF						
(mg/1)	(mg/l)	WATER	0.37 (0.35) 0.42 (0.40) 0.43 (0.39)	FILTER	LAB	TOTAL				
0.0 0.5 1 2 4 6 Low Fe	0.14 (0.13) 0.10 (0.07) 0.09 (0.07) 0.16 (0.14) 0.10 (0.13) 0.13 (0.09) 0.12 (0.13)	0.94 0.86 1.05 0.96 0.81 0.86 0.90	0.37 (0.35) 0.42 (0.40) 0.43 (0.39) 0.54 (0.32) 0.53 (0.29)	0.41 (0.42) 0.41 (0.39) 0.58 (0.60) 0.47 (0.53) 0.41 (0.38)	0.07 (0.06) 0.11 (0.12) 0.13 (0.15) 0.11 (0.10) 0.17 (0.14) 0.11 (0.10) 0.07 (0.07)	0.52 (0.54) 0.54 (0.54) 0.69 (0.70) 0.64 (0.67) 0.52 (0.48)				

Table B2b.16 - Adsorbable organic halide (AOX) (ug/l)

OZONE DOSE	NON HAND CHLORINATED	HAI	HAND CHLORINATED							
(mg/l)	2° RGF	RAW	1° RGF	2° RGF						
1 2 4 Low Fe	13.9 (36.1) 20.8 (37.4) 18.4 (36.6) 18.4 (22.1)	48.9 66.9 62.8 61.6	16.9 (56.9) 28.3 (32.0) 20.5 (60.1) 20.9 (21.9)	59.3 (62.9) 37.0 (43.3) 26.3 (74.3) 20.3 (31.8)						

Table B2b.17 - Mutagenic activity (slope value)

OZONE	NON	1 CHL	ORINATI	ED		HAND	CHLOR	INATEI) FINA	AL WA	TER	
	TF	RIAL	1° RGI	יז	TRIAL STREAM				CONTROL STRAM			
DOSE (mg/l)	TA 98 TA			100	TA	98	TA 100		TA	98	TA 100	
(1119/1)	рН 2	рн 7	pH 2	рН 7	pH 2	рН 7	рн 2.	рН 7	рН 2	рН 7	рН 2	рН 7
4	0.37	0.77	0.01	0.24	2.43	1.41	15.70	8.97	3.19	5.15	15.75	16.84

PHASE II. TRIAL 3a. EFFECT OF INTERFILTRATION OZONATION (FIXED pH)

During this trial, pH control was generally good. However, there were a couple of runs where the accuracy of the 1° filtrate pH measurement was suspect. It is thought that the pH of the 1° filtrate during the second half of the trial, at ozone doses of 0.3 and 0.6 mg/l, were much higher than quoted in table B3a.2 (the actual values were probably between 7 and 8). There were also a number of occasions when the 2° filtrate pHs dropped (on one occasion as low as 7.2), and on these occasions, the sample pH was adjusted to 9.0, in the lab, before hand chlorination.

The additional 2° filters were commissioned for this trial, one in each stream contained "new" sand and the other contained the "old", conditioned sand; in the results tables the two filters are therefore neaded "OLD" or "NEW".

Table B3a.1 - Chemical doses

	FERRIC	·	OZO	ONATEI	STREA	AM		CHLORINATED STREAM				
DATE DOSE (mg/l)		DOSE (mg/l)		CONTACT TIME		DPD RESIDUAL		DOSE (mg/l)		RESIDUAL (mg/l)		
24.		NEW	OLD	NEW	OLD	NEW	OLD	NEW	OLD	NEW	OLD	
25 Jan 90 30 Jan 90 6 Feb 90 13 Feb 90 20 Feb 90 6 Mar 90 13 Mar 90 20 Mar 90	3.8 3.7 4.1 2.7 2.6 2.5 2.1 2.1	0.6 0.4 2.5 5.0 1.2 5.0 0.6 0.3	0.6 0.4 2.5 5.0 1.2 5.0 0.7	8 8 8 RGF RGF RGF	8 8 8 15 15 15	- 4.9 0.9 0.4 0.0	5.1 5.0 3.8 1.6	0.44 0.39 0.41 0.42 0.47 0.00 0.00	0.44 0.39 0.41 0.42 0.47 0.48 0.43	0.09 0.16 0.13 0.14 0.08 0.00 0.00	0.08 0.06 0.05 0.04 0.04 0.08 0.06 0.09	

Table B3a.2 - pHs

OZO	NATION	RAW		1°	RGF		2° I	RGF	
DOSE (mg/l)	TIME (mins)	WATER	DAF	03	Cl	New03	01d03	NewCl	OldCl
0.4	8, 8	4.8	4.5	6.5	6.6	9.0	8.9	8.9	8.9
0.6	8, 8	5.0	4.7	6.6	6.6	8.9	8.9	9.0	8.9
2.5	8, 8	4.8	4.6	6.7	6.7	8.3	9.0	9.1	9.1
5.0	8, 8	4.7	4.6	6.7	6.8	9.0	9.0	9.0	7.1
0.3	RGF,15	4.9	4.6	6.8	6.9	9.0	9.0	9.1	9.1
0.6	RGF,15	4.8	4.7	6.7	6.6	8.9	8.9	9.1	9.1
1.2	RGF,15	4.8	4.6	6.7	6.6	9.0	7.2	8.7	8.8
5.0	RGF,15	4.8	4.6	6.5	6.5	8.9	8.6	8.8	8.9

Table B3a.3 - Colour: °Hazen (= Abs/m @400nm * 11)

OZON	NOITA	RAW WATER		DAF		1°RGF			2°RGF		
DOSE (mg/l)	TIME (mins)	APP	TRUE	APP	TRUE	03	Cl	New03	01d03	NewCl	oldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	46 40 43 38	21 21 20 21	25 21 19 23	3 4 3 4	2 2 3 3	2 3 3 2	15 11 8 8	15 16 8 9	3 3 4 3	3 3 4 2
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	30 33 40 35	12 14 16 14	16 21 20 21	2 4 3 4	5 4 2 3	5 4 2 3	4 5 2 3	8 11 12 9	5 5 3 3	5 5 3 4

Table B3a.4 - uv Absorbance (Abs/m @ 254nm)

OZON	IATION	RAW WATER		DAF		. 1°RGF		2° RGF			
DOSE (mg/l)	TIME (mins)	APP	TRUE	APP	TRUE	03	Cl	New03	01d03	NewCl	oldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	22.2 21.6 21.2 21.0	17.1 17.2 16.0 16.0	11.8 11.4 10.0 11.3	4.0 4.1 3.6 4.2	3.4 3.5 3.8 4.3	3.5 3.7 3.8 4.2	4.2 3.3 2.4 2.5	3.9 3.6 2.6 2.5	3.6 3.9 3.9 4.1	3.5 4.0 4.2 4.2
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	16.6 17.6 20.1 18.4	11.8 13.3 15.2 13.6	9.2 10.3 11.1 10.7	3.6 4.0 4.1 4.2	6.1 5.5 3.7 3.5	6.1 5.6 3.8 3.4	5.1 4.9 2.4 2.0	5.6 5.1 3.2 2.0	5.5 5.3 3.6 3.5	5.4 5.2 3.8 3.4

Table B3a.4b - Ozonated 2° RGF samples before and after membrane filtration

OZO	NATION	BEF	ORE M	EMBRA	NE FI	LTRAT	ION	AFTER MEMBRANE FILTRATION					
DOSE (mg/l)	TIME (mins)	NEW SAND		OL	OLD SAND			NEW SAND			OLD SAND		
			UV Ab/m	Mn mg/l	COL DegH	UV Ab/m	Mn mg/l	COL DegH	UV Ab/m	Mn mg/l	COL DegH	1	Mn mg/l
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	15 11 8 8	2.4	0.09	15 16 8 9	3.9 3.6 2.6 2.5	0.10	8 - 7 6	3.5 - 2.3 1.8	-	6 - 7 7	2.8	0.03
0.3 0.6 1.2 5.0	RGF, 15 RGF, 15 RGF, 15 RGF, 15	4 5 2 3	4.9 2.4	0.01 0.01 0.02 0.01	8 11 12 9	5.1	0.07 0.08 0.17 0.12	- - -	-	-	4 7 4 7	4.5	0.05 0.05 0.07 0.08

Table B3a.5 - Turbidity (NTU)

OZONATION			_	1° RGF		2° RGF			
DOSE (mg/l)	TIME (mins)	RAW WATER	DAF	03	Cl	New03		NewCl	OldCl
0.4	8, 8	4.9	1.7	0.1	0.1	0.9	1.1	0.1	0.1
0.6	8, 8	2.8	1.2	0.1	0.1	0.7	1.0	0.1	0.1
2.5	8, 8	4.1	1.2	0.1	0.1	0.2	0.2	0.1	0.2
5.0	8, 8	3.8	1.6	0.2	0.2	0.2	0.2	0.1	0.1
0.3	RGF,15	2.4	1.1	0.3	0.3	0.2	0.2	0.2	0.2
0.6	RGF,15	2.8	1.3	0.2	0.2	0.2	0.2	0.2	0.2
1.2	RGF,15	4.2	1.5	0.1	0.1	0.1	0.2	0.1	0.1
5.0	RGF,15	3.5	1.8	0.1	0.1	0.1	0.3	0.1	0.1

Table B3a.6 - Iron (mg/l)

OZONATION		RAW		1° RGF		2° RGF			
DOSE (mg/l)	TIME (mins)	WATER	i i	03	Cl	New03	01d03	NewCl	OldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	0.48 0.38 0.40 0.38	1.28 0.96 0.90 1.00	0.03 0.02 0.03 0.03	0.02 0.02 0.03 0.04	0.02 0.02 0.03 0.02	0.02 0.02 0.03 0.02	0.02 0.02 0.01 0.01	0.02 0.04 0.01 0.04
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	0.32 0.32 0.36 0.32	0.78 0.90 1.01 0.99	0.12 0.08 0.02 0.02	0.13 0.08 0.03 0.01	0.08 0.06 0.03 0.01	0.08 0.04 0.01 0.01	0.07 0.05 0.03 0.01	0.08 0.06 0.01 0.01

Table B3a.7 - Manganese (mg/l)

OZONATION		RAW		1° RGF		2° RGF				
DOSE (mg/l)	TIME (mins)	WATER	t	DAF	03	Cl	New03	01d03	NewCl	OldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	0.18 0.19 0.18 0.18	0.20 0.22 0.19 0.19	0.20 0.23 0.26 0.28	0.22 0.24 0.27 0.26	0.13 0.09 0.09 0.14	0.12 0.10 0.09 0.14	0.01 0.01 0.00 0.00	0.00 0.02 0.00 0.01	
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	0.17 0.18 0.18 0.18	0.19 0.19 0.21 0.20	0.19 0.18 0.25 0.25	0.17 0.18 0.25 0.24	0.01 0.01 0.02 0.01	0.07 0.08 0.17 0.12	0.00 0.00 0.01 0.00	0.00 0.00 0.01 0.00	

Table B3a.8 - Aluminium (mg/l)

OZO	NATION	RAW		1° 1	RGF		2° :	RGF	
DOSE (mg/l)	TIME (mins)	WATER 0.36	DAF	03	Cl	New03	01d03	NewCl	OldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	0.36 0.38 0.51 0.36	0.27 0.32 0.33 0.30	0.01 0.01 0.05 0.08	0.03 0.03 0.06 0.07	0.03 0.03 0.05 0.10	0.03 0.03 0.05 0.10	0.03 0.03 0.05 0.10	0.04 0.07 0.07 0.12
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	0.35 0.54 0.41 0.37	0.25 0.28 0.39 0.30	0.19 0.14 0.01 0.04	0.21 0.12 0.03 0.02	0.19 0.12 0.08 0.04	0.19 0.13 0.05 0.06	0.19 0.12 0.02 0.04	0.18 0.11 0.12 0.04

Table B3a.9 - Total Organic Carbon (mg/l)

020	NATION	D3***			: :	
DOSE (mg/l)	TIME (mins)	RAW WATER	New03	1	RGF NewCl	OldCl
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	4.46 4.40 4.08 3.83	1.75 1.63 1.65 1.31	1.79 1.93 1.79 1.42	1.69 1.93 2.28 1.65	1.82 1.92 1.96 1.74
0.3 0.6 1.2 5.0	RGF, 15 RGF, 15 RGF, 15 RGF, 15	3.93 3.71 3.42 3.35	1.87 2.07 1.56 1.72	1.84 1.91 1.51 1.29	2.27 1.94 1.55 1.59	1.95 1.89 1.69 1.86

Table B3a.10 - Hand Chlorinated Final Water Bacteriological Quality (Total Coliforms, E-Coli per 100 ml); 37°C 1-Day Colonies, 22°C 3-Day Colonies (per ml

OZO	NATION	OZONA	TED	CHLORI	INATED
DOSE (mg/l)	TIME (mins)	NEW SAND	OLD SAND	NEW SAND	OLD SAND
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8	0, 0, 0, 0 0, 0, 0, 0 0, 0, 0, 0 0, 0, 1, 2	0, 0, 0, 0 0, 0, 0, 0 0, 0, 1, 2 0, 0, 0, 1	0, 0, 0, 0 0, 0, 1, 4 0, 0, 0, 0 0, 0, 4, 5	0, 0, 0, 0 0, 0, 1, 0 0, 0, 1, 1 0, 0, 2, 1
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	0, 0, 0, 0 0, 0, 0, 5 0, 0, 0, 0 0, 0, 0, 0	0, 0, 0, 6 L O S T 0, 0, 0, 0 0, 0, 1, 0	0, 0, 1, 7 0, 0, 0,183 0, 0, 0, 1 0, 0, 0, 4	0, 0, 1, 1 0, 0, 0, 34 0, 0, 1, 2 0, 0, 0, 0

Table B3a.11 - Chloroform (ug/l)

OZO	NOITAN	NON I	HAND CI		ATED	I	ANI	ОСІ	LOF	RINI	ATEI) 	
DOSE	TIME		2°	RGF		RAW	1° I	RGF		2° 1	RGF		
mg/l	mins	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl	
0.4 0.6 2.5 5.0	8,8 8,8 8,8 8,8	2.00 <0.13 4.62 0.97	1.60 <0.13 4.51 6.75	3.00 <0.13 7.33 3.23	<0.13 8.04	31.40 35.00 32.53 0.92	9.50 4.50 12.22 7.23	5.00 12.35	6.90 1.00 9.54 3.88	7.20 1.20 10.06 3.55	13.28		*
0.3 0.6 1.2 5.0	RGF15 RGF15 RGF15 RGF15	<0.13 <0.13 2.85 5.78	<0.13 <0.13 2.77 5.73	<0.13 6.63	<0.13 5.40	20.73 19.27 17.47 17.35	6.68 4.05 7.90 8.97	4.82 7.72	3.12 2.85 5.38 7.76	4.44	4.76 10.38	7.58 8.04 9.67 9.92	#

^{*} Analysed 4 days after sampling # Analysed 3 days after sampling

Table B3a.12 - Bromodichloromethane (ug/1)

OZO	NATION	NON	HAND C		ATED		H A N	D C	H L O 1	RIN.	ATE	D	
DOSE	TIME		7	RGF	<u> </u>	RAW	1°	RGF		ź° :	RGF		
mg/l	mins	New03	01d03	NewCl	01dC1	WATER	03	Cl	New03	01d03	NewCl	oldCl	1
0.4 0.6 2.5 5.0	8,8 8,8 8,8	<0.01 <0.01 0.58 <0.01	<0.01 0.60	<0.01 0.60	<0.01 0.57	0.50 0.90 1.11 <0.01	0.10 0.87	1.20 0.10 0.89 0.85	0.10 0.10 0.90 0.80	1.00 0.10 0.94 0.81	0.20	0.40 0.20 0.94 0.95	*
0.6	RGF15 RGF15 RGF15 RGF15	<0.01 <0.01 <0.01 1.20	<0.01 <0.01 <0.01 <0.01	<0.01 <0.01 1.31 1.19	<0.01 <0.01 0.76 1.21	<0.01 <0.01 1.12 1.40		<0.01 <0.01 0.88 1.31	<0.01 <0.01 0.88 1.31	<0.01 <0.01 0.87 1.39	<0.01 <0.01 1.79 1.36	<0.01 <0.01 0.99 1.38	#

^{*} Analysed 4 days after sampling # Analysed 3 days after sampling

Table B3a.13 - Dibromochloromethane (ug/l)

ozo	NATION	NON	HAND C	HLORIN. RGF	ATED		H A N	D C	H L O	RIN.	A T E	D
DOSE	TIME			NGE	_	RAW	l°:	RGF		2° :	RGF	
mg/l	mins	New03	01d03	NewCl	OldCl	WATER	03	Cl	New03	01d03	NewCl	oldCl
0.4 0.6 2.5 5.0	8,8 8,8 8,8 8,8	<0.05	<0.05 <0.05 <0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05	<0.05	0.12	0.10	0.06	0.12	<0.05
0.3 0.6 1.2 5.0	RGF15 RGF15 RGF15 RGF15	<0.05 <0.05	<0.05 <0.05 <0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05	<0.05 <0.05	<0.05 <0.05

^{*} Analysed 4 days after sampling # Analysed 3 days after sampling

Table B3a.14 - Bromoform (ug/1)

OZOI	NOITAN	NON I	HAND CI	HLORINI RGF	ATED	I	H A N I	C F	LOF	RINA	ATEI)	
DOSE	TIME		Jew03 01d03 NewCl 01d0			RAW	1° I	RGF		2° F	RGF		
mg/l	mins	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	oldCl	
0.4 0.6 2.5 5.0	8,8 8,8 8,8 8,8	•	<0.03 <0.03	<0.03	<0.03 <0.03	<0.03 <0.03 0.08 <0.03	<0.03	<0.03	<0.03	<0.03 0.06	1 .	<0.03	*
0.3 0.6 1.2 5.0	RGF15 RGF15 RGF15 RGF15	<0.03 <0.03 <0.03 <0.03	<0.03 <0.03 <0.03 <0.03	<0.03	<0.03	<0.03	<0.03 <0.03	<0.03 <0.03 <0.03 <0.03	<0.03 <0.03	<0.03 <0.03	<0.03	<0.03 <0.03	#

^{*} Analysed 4 days after sampling # Analysed 3 days after sampling

Table B3a.15 - Total Trihalomethanes (ug/l)

OZO	NOITAN	NON I	HAND CH	LORINA RGF	ATED	I	ANI) C I	LOF	RINZ	ATEI)	
DOSE	TIME		New03 01d03 NewC1 01d0			RAW	1° I	RGF		2° I	RGF		
mg/l	mins	New03	01d03	NewCl	OldCl	WATER	03	Cl	New03	01d03	NewCl	oldCl	
0.4 0.6 2.5 5.0	8,8 8,8 8,8 8,8	2.09 <0.22 5.28 1.06	1.69 <0.22 5.19 6.84	3.09 <0.22 8.01 4.01	<0.22	31.98 35.98 33.78 1.01	4.68	5.25 13.39	7.08 1.23 10.67 4.76	8.28 1.43 11.12 4.44	7.85 14.23		*
0.3 0.6 1.2 5.0	RGF15 RGF15 RGF15 RGF15	<0.22 <0.22 2.94 7.06	<0.22 <0.22 2.86 5.82		<0.22 6.24	20.82 19.36 18.67 18.83	4.14 8.88	1	3.21 2.94 6.34 9.15	2.55 1.84 5.39 8.73	4.85 12.25	8.13	#

^{*} Analysed 4 days after sampling # Analysed 3 days after sampling

Table B3a.16 - Chlorine demand (mg/l)

OZO	NATION		С	H L O	RIN	E D	ЕМА	N D	(mg/l)	·
DOSE	TIME	W R A A T	1° 1	RGF	NI	CHL EW SA	ORINATI	· · · ·	RGF LD SA	ND	OZON. 2°	ATED RGF
mg/l	(mins)	W E	03	Cl	RGF	Lab	Total	RGF	Lab	Total	New Sand	Old Sand
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8 8, 8	0.85 0.89 0.83 0.82	0.31 0.31 0.32 0.32	0.28 0.31 0.32 0.31	0.23 0.35 0.28 0.28	0.06 0.07 0.06 0.12	0.29 0.42 0.34 0.40	0.33 0.36 0.36 0.38	0.06 0.08 0.06 0.09	0.39 0.44 0.42 0.47	0.23 0.17 0.13 0.07	0.17 0.20 0.13 0.04
0.3 0.6 1.2 5.0	RGF,15 RGF,15 RGF,15 RGF,15	0.67 0.63 0.73 0.63	0.37 0.26 0.25 0.23	0.33 0.27 0.26 0.21	0.00 0.00 0.39 0.00	0.31 0.26 0.06 0.23	0.31 0.26 0.45 0.23	0.37 0.37 0.43 0.40	0.13 0.06 0.03 0.08	0.50 0.43 0.46 0.48	0.28 0.29 0.29 0.21	0.20 0.10 0.05 0.02

Table B3a.17 - Adsorbable organic halide (AOX) (ug/l)

OZO	NATION	NON	HAND C	HLORIN RGF	ATED	1	ANI	D C	H L O 1	RIN.	ATE) .
DOSE	TIME					RAW	l° I	RGF		2° :	RGF	
mg/l	(mins)	New03 Old03 NewCl OldC				WATER	03	Cl	New03	01d03	NewCl	OldC1
0.4 0.6 2.5 5.0	8, 8 8, 8 8, 8 8, 8	15.7 8.3 14.5 13.0	9.7 <8 29.6 <8	17.8 18.1 20.9 14.3	20.5 20.8 24.8 26.8		21.8 27.2 29.6 66.6	44.6 30.5	10.5 13.7	13.5 15.7 9.3 <8	28.0 31.6 31.9 21.9	31.3 26.8 31.0 28.2
5.0	RGF,15	<8	<8	9.1	20.1	59.8	22.6	19.8	96.5	13.1	26.7	23.1

Table B3a.18 - TA 98 Mutagenic activity (slope value)

OZ	OATION	OZ	ONATED	2° 1	RGF	CHLO	RINATE) 2°	RGF
DOSE	TIME	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND
mg/l	(mins)	рн 2	рн 7	рн 2	рН 7	рН 2	рН 7	рн 2	рН 7
0.4 5.0	8, 8 8, 8	1.67 0.42	2.63 -0.39		2.67 0.91	3.61 5.22	4.55 5.70	3.18 2.44	4.01 5.42
5.0	RGF,15	0.77	1.04	1.08	0.28	3.62	3.65	3.14	4.90

Table B3a.19 - TA 100 Mutagenic activity (slope value)

OZ	OATION	OZ	ONATED	2° 1	RGF	CHLO	RINATEI) 2°	RGF
DOSE	TIME	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND
mg/l	(mins)	рн 2	рн 7	рН 2	рн 7	рН 2	рн 7	рн 2	рн 7
0.4 5.0	8, 8 8, 8	6.08 5.21	5.46 2.50				15.34 10.94		
5.0	RGF,15	12.79	4.84	6.15	2.84	18.16	14.81	17.23	15.68

PHASE II. TRIAL 3b. EFFECT OF INTERFILTRATION OZONATION PH

PILOT PLANT CONTROL

The DAF and 1° filtrate pH control were reasonable during this trial. Because ozonation reduced the pH of the water the 2° filtrate pHs did not cover the target range very evenly: most of the values were grouped at the lower end of the range. The pH of each sample was adjusted to 9.0 in the lab before hand chlorination.

Table B3b.1 - Chemical Doses

		FERRIC		OZ	OŅATEI	STRE	MA		CHLO	ORINATE	ED STRE	EAM
	DATE	DOSE (mg/l)	DOS (mg)		CON?	FACT EME	_	PD DUAL	DOS (mg/			DUAL
6.5	-		NEW	OLD	NEW	OLD	NEW	OLD	NEW	OLD	NEW	OLD
2	3 Apr 9	2.6 30 2.0 30 1.8 30 1.5	1.2 1.9 2.1 1.7	1.2 1.2 2.4 2.2	RGF RGF RGF RGF	15 15 15 15	0.9 1.1 5.0 3.5	5.0 0.0 0.0 4.5	0.47 0.00 0.00 0.00	0.47 0.57 0.53 0.59	0.08 0.00 0.00 0.00	0.04 0.09 0.04 0.07

Table B3b.2 - pH

DATE	RAW WATER DAF		1° RGF			2° RGF				
	WHIEN	DAT	03	Cl	New03	01d03	NewCl	OldCl		
20 Feb 90 27 Mar 90 3 Apr 90 10 Apr 90	4.8 4.9 5.2 5.2	4.6 4.7 4.8 4.8	6.7 6.1 6.5 6.3	6.6 6.2 6.4 6.3	9.0 5.9 6.6 7.2	7.2 5.7 6.6 7.0	8.7 9.3 8.8 8.8	8.8 6.1 6.9 6.8		

Table B3b.3 - Colour: °Hazen (= Abs/m @400nm * 11)

NEW OZONE pH	RAW WATER		DAF		1°RGF		2°RGF				
F	APP	TRUE	APP	TRUE	03	Cl	New03	01d03	NewCl	OldCl	
5.9 6.6 7.2 9.0	37 26 25 40	11 11 9 16	17 18 16 20	თ თ თ თ	2 3 3 2	2 2 3 2	19 2 2 2	11 11 12 12	2 4 4 3	1 3 3 3	

Table B3b.4a - uv Absorbance (Abs/m @ 254nm)

NEW OZONE pH	RAW WATER		DAF		1°RGF		2° RGF				
P.1	APP	TRUE	APP	TRUE	03	Cl	New03	01d03	NewCl	oldCl	
5.9 6.6 7.2 9.0	17.4 15.4 15.1 20.1	10.4 10.3 9.5 15.2	9.4 9.2 9.7 11.1	3.4 3.7 3.8 4.1	2.7 3.8 3.6 3.7	2.7 3.6 3.7 3.8	2.7 2.4 2.2 2.4	1.7 2.6 2.9 3.2	2.9 4.0 3.8 3.6	2.2 3.9 3.5 3.8	

Table B3b.4b - Ozonated 2° RGF samples before and after membrane filtration

T				_							TTTCI	
BEF	ORE M	IEMBRA	NE FI	LTRAT	ION	AF	TER M	EMBRA	NE FI	 Ј.Фрап	TON	
NE	W SAN	D	OLD SAND			1			Ţ ~ ~			
COL DegH	UV Ab/m	Mn mg/l	COL DegH	UV Ab/m	Mn mg/l	COL	UV	Mn	COL	UV	Mn	
19	2.7	0.18	11						DegH	Ab/m	mg/l	
2 2 2	2.2	0.02	11 12 12	2.6	0.07 0.18	8 2 2 -	2.5	0.03	1 6 10 4	_ [0.03 0.01 0.14 0.07	
	COL DegH	NEW SAN COL UV DegH Ab/m 19 2.7 2 2.4 2 2.2	NEW SAND COL UV Mn Ab/m mg/1 19 2.7 0.18 2 2.4 0.08 2 2.2 0.02	NEW SAND OL COL UV Mn COL DegH Ab/m mg/l DegH 19 2.7 0.18 11 2 2.4 0.08 11 2 2.2 0.02 12	NEW SAND OLD SAN COL UV Mn COL UV DegH Ab/m mg/1 DegH Ab/m 19 2.7 0.18 11 1.7 2 2.4 0.08 11 2.6 2 2.2 0.02 12 2.9 2 2 4 0.03 13 2.6	COL UV Mn COL UV Mn mg/l DegH Ab/m mg/l 19 2.7 0.18 11 1.7 0.10 2 2.4 0.08 11 2.6 0.07 2 2.2 0.02 12 2.9 0.18	NEW SAND OLD SAND NE COL UV Mn COL UV Mn mg/l DegH Ab/m mg/l DegH 19 2.7 0.18 11 1.7 0.10 8 2 2.4 0.08 11 2.6 0.07 2 2 2.2 0.02 12 2.9 0.18 2	NEW SAND OLD SAND NEW SAN COL UV Mn COL UV Mn mg/l DegH Ab/m mg/l DegH Ab/m mg/l DegH Ab/m mg/l DegH Ab/m 19 2.7 0.18 11 1.7 0.10 8 2.0 2 2.4 0.08 11 2.6 0.07 2 2.5 2 2.2 0.02 12 2.9 0.18 2 1.9	NEW SAND OLD SAND NEW SAND COL UV Mn COL UV Mn mg/l DegH Ab/m mg/l DegH Ab/m mg/l DegH Ab/m mg/l DegH Ab/m mg/l 19 2.7 0.18 11 1.7 0.10 8 2.0 0.11 2.6 0.07 2 2.5 0.03 2 2.4 0.02 12 2.9 0.18 2 1.9 0.02	BEFORE MEMBRANE FILTRATION AFTER MEMBRANE FI NEW SAND OLD SAND NEW SAND OLD OLD SAND COL UV DegH Ab/m mg/1 Mn COL UV Mn mg/1 COL UV Mn mg/1 COL UV Mn mg/1 COL DegH Ab/m mg/1 DegH DegH 19 2.7 0.18 11 1.7 0.10 8 2 2.4 0.08 11 2.6 0.07 2 2.5 0.03 6 2 2.2 0.02 12 2.9 0.18 2 1.9 0.02 10 2 2.4 0.02 12 3.2 0.17 -	NEW SAND OLD SAND NEW SAND OLD SAND COL UV DegH Ab/m mg/l DegH Ab/m COL UV Mn COL UV Mn COL UV Mn mg/l DegH Ab/m mg/l DegH Ab/m mg/l DegH Ab/m 19 2.7 0.18 11 1.7 0.10 8 2.4 0.08 11 2.6 0.07 2 2.5 0.03 6 1.8 2 2.2 0.02 12 2.9 0.18 2 1.9 0.02 10 2.5 2 2.4 0.02 12 3.2 0.17 -	

Table B3b.5 - Turbidity (NTU)

						-	,	,
NEW OZONE PH	RAW WATER	DAF	1°			2°	RGF	
			03	Cl	New03	01d03	NewC1	01dC1
5.9 6.6 7.2 9.0	4.0 1.8 1.7 4.2	1.2 1.0 1.0 1.5	0.1 0.1 0.1 0.1	0.1 0.1 0.1 0.1	0.5 0.1 0.1 0.1	0.4 0.1 0.2 0.2	0.1 0.1 0.1 0.1	0.1 0.1 0.1 0.1

Table B3b.6 - Iron (mg/1)

									
NEW OZON		RAW		1° R	GF			GF	
pH		WATER	DAF	03	Cl	New03	01d03	 	
5.5 6. 7. 9.	6 2	0.45 0.25 0.25 0.36	0.72	0.02 0.01 0.01 0.02	0.03 0.01 0.02 0.03			0.03 0.01 0.01 0.03	

Table B3b.7 - Manganese (mg/l)

								
NEW OZONE	RAW		1° R	GF			GF	
pН	WATER	DAF	03	Cl	New03	01d03		
5.9 6.6 7.2 9.0	0.17 0.20 0.18 0.18		0.19 0.19 0.19 0.25	0.19 0.20 0.19 0.25	0.08	0.10 0.07 0.18 0.17	0.00 0.00 0.01 0.01	0.03 0.02 0.00 0.01

Table B3b.8 - Aluminium (mg/l)

NEW OZONE	RAW		1° F	RGF		2° F	RGF	
Hq	WATER	DAF	03	Cl	New03	01d03	NewCl	oldCl
5.9 6.6 7.2 9.0	0.38 0.33 0.33 0.41	0.29 0.26 0.24 0.39	0.03 0.01 0.03 0.01	0.01 0.01 0.03 0.03	0.01 0.16 0.03 0.08	0.02 0.00 0.02 0.05	0.03 0.06 0.03 0.02	0.01 0.02 0.02 0.12

Table B3b.9 - Total Organic Carbon (mg/l)

NEW OZONE	RAW WATER		2° F	RGF	
DOSE (mg/l)	WAIEK	New03	01d03	NewCl	OldCl
5.9 6.6 7.2 9.0	3.39 3.26 3.22 3.42	1.30 1.79 1.71 1.56	1.29 1.30 1.42 1.51	1.59 1.69 1.45 1.55	1.23 2.08 1.73 1.69

Table B3b.10 - Hand Chlorinated Final Water Bacteriological Quality (Total Coliforms, E-Coli (per 100 ml); 37°C 1-Day Colonies, 22°C 3-Day Colonies (per ml)

NEW OZONE pH	OZONA	TED	CHLORINATED				
	NEW SAND	OLD SAND	NEW SAND	OLD SAND			
5.9 6.6 7.2 9.0	0, 0, 2, 1 0, 0, 2, 1 0, 0, 0,24 0, 0, 0, 0	0, 0, 1, 0 0, 0, 1, 5 0, 0, 0, 2 0, 0, 0, 0	0, 0, 0,52 0, 0, 4, 0 0, 0, 2, 3 0, 0, 0, 1	0, 0, 0, 2 0, 0, 5,17 0, 0, 0, 0 0, 0, 1, 2			

Table B3b.11 - Chloroform (ug/1)

NEW	NON	HAND C	HLORIN. RGF	ATED	I	H A N I) C	HLORINATED				
OZONE pH					RAW	1° 1	RGF		2° :	RGF		
	New03	01d03	NewCl	OldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl	
5.9 6.6 7.2 9.0		<0.13 <0.13		2.20 <0.13	22.5 23.72 20.74 17.47	<0.1 4.03 6.50 7.90	8.7 3.90 9.87 7.72	<0.1 2.67 3.77 5.38	5.0 4.11 4.36 4.44	5.0 5.63 7.57 10.38	10.3 12.46 11.04 9.67	

^{*} Analysed at Broughton

Table B3b.12 - Bromodichloromethane (ug/l)

NEW	NON I	HAND CI	HLORINA RGF	ATED	F	ANI) C I	HLOF	RINI	ATEI)	
ÖZONE			NGF		RAW	1° F	RGF		2° 1	RGF		
E PII	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl	
5.9 6.6 7.2 9.0	<0.01 <0.01	1	1	<0.01	0.46 0.58	<0.01 0.28	<0.01 0.97	0.32 0.32	0.56	0.48	4.3 1.21 1.75 0.99	1

^{*}Analysed at Broughton

Table B3b.13 - Dibromochloromethane (ug/1)

NEW	NON I	HAND CI	HLORIN RGF	ATED]	HANI) C	HLOI	RINA	A T E 1)	
OZONE pH			INGI		RAW	l° I	RGF		2° 1	RGF		
Pii	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl	
5.9 6.6 7.2 9.0	<0.1 <0.05 <0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 0.12	<0.05 <0.05	0.11		0.11	

^{*}Analysed at Broughton

Table B3b.14 - Bromoform (ug/1)

NEW	NON	HAND CI 2°	HLORIN RGF	ATED	1	HANI	O C 1	HLOI	RINA	ATEI)	
OZONE pH	_				RAW	1° 1	RGF		2° 1	ŔĠF		
Pi	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	oldCl	
5.9 6.6 7.2 9.0	<0.03 <0.03	<0.03	<0.03 <0.03	<0.03 <0.03	<0.03	<0.03	<0.03	<0.1 <0.03 <0.03 <0.03	<0.03	<0.03	ł	7

^{*}Analysed at Broughton

Table B3b.15 - Total trihalomethanes (ug/l)

NEW	NON	HAND CI	HLORIN RGF	ATED	I	HANI) C 1	HLOI	RINI	ATEI) ·
OZONE pH			1.02		RAW	l° I	RGF		2° 1	RGF	
P.1	New03	01d03	NewCl	oldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl
5.9 6.6 7.2 9.0	<0.22	<0.22 <0.22	<0.22	2.29	22.8 24.26 21.40 18.67	<0.4 4.12 6.86 8.88	ı	<0.4 3.07 4.17 6.34	5.3 5.04 5.06 5.39	5.82 8.13	14.8 13.81 13.08 10.74

^{*}Analysed at Broughton

Table B3b.16 - Chlorine demand (mg/l)

			C	H _L O	RIN	E D	E M A	N D	(m	ng/l)		
NEW	Б	W	1° R	GF	CHLORINATED 2° RGF							TED RGF
OZONE	Α	A	1 1	.01	NEW SAND OLD SAND						New	Old
⊹ pH	W	E R	03	Cl	RGF	Lab	Total	RGF	Lab	Total	Sand	Sand
5.9 6.6 7.2 9.0	0	.80 .69 .74	0.31 0.25 0.35 0.25	0.29 0.25 0.30 0.26	0.00 0.00 0.00 0.39	0.35 0.27 0.37 0.06	0.35 0.27 0.37 0.45	0.48 0.49 0.52 0.43	0.21 0.16 0.22 0.03	0.69 0.65 0.74 0.46	0.37 0.62 0.41 0.29	0.65 0.96 0.54 0.05

Table B3b.17 - Adsorbable organic halide (AOX) (ug/l)

	NON I		LORINA	ATED	I	ANI) C I	LOF	RINA	TEI)
NEW OZONE		2°	RGF		RAW	1° F	RGF		2° I	RGF	
рH	New03	01d03	NewCl	OldCl	WATER	03	Cl	New03	01d03	NewCl	OldCl
5.9	8.9	9.5 <8	<8 <8	39.0 35.6	53.8 71.6	49.1 29.1	27.8 27.3	8.5 11.9	13.6 12.8	37.1 30.7	29.9 44.2

Table B3b.18 - TA 98 Mutagenic activity (slope value)

NEW	OZ	ONATED	2° :	RGF	CHLO:	RINATE	D 2°	RGF
OZONE pH	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND
	рН 2	рН 7	рН 2	рН 7	рН 2	рН 7	рН 2	рн 7
5.9	1.46	1.76	1.13	1.38	2.27	3.50	2.39	5.14

Table B3b.19 - TA 100 Mutagenic activity (slope value)

NEW	OZ	ONATED	2° :	RGF	CHLO	RINATE	D 2°	RGF
OZONE pH	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND.
	рН 2	рН 7	рН 2	рн 7	рН 2	рН 7	рН 2	рН 7
5.9	9.18	11.40	3.20	6.30	16.79	15.65	17.85	20.89

TRIAL B3bR (REPEAT) - EFFECT OF OZONATION AND CHLORINATION PH

Because of the poor results from the runs investigating effect of ozonation pH, it was decided to carry out a single run to investigate ozonation pH and chlorination pH. For this run, one DAF was run without pH adjustment before the 1% RGF. The 1° RGF filtrate was then dosed with caustic before being pumped to the ozone contactors. The ozonated water was not passed through a 2° RGF prior to sampling.

Five nominal ozonation/chlorination pHs were chosen, 5, 6, 7, 8 and 9. These were the target pHs from the ozone contactor, and ozonated waters were then hand chlorinated both without further pH adjustment, and with pH adjustment to 9 in the lab. samples of 1° RGF filtrate were also pH adjusted in the lab, to enable hand chlorination (of un-ozonated water), at the target pHs.

RESULTS

Table B3bR.1a - Non hand chlorinated samples

		Mar	n 1	TOC	COT	OUR	Ţ	JV	Hq	TURB
Sample	Fe mg/l	Mn mg/l	Al mg/l	mg/l	App Hazen	True Hazen	11	True Abs/m	•	NTU
RAW DAF 1'RGF	0.25 0.77 0.03	0.19 0.20 0.36	0.24 0.09 0.02	<u>-</u>	22 - 13 2	7 2 -	11.6 7.2 2.5	7.2 2.9	5.5 5.4 6.4	1.7 0.8 0.1

Table B3bR.1b - Hand chlorinated raw water

i	ClDem	Tr	ihalom	ethane:	s (ug/	1)	2011
	mg/l	C13	Cl2Br	ClBr2	Br3	Total	AOX ug/l
	0.86	21.19	1.08	<0.05	<0.03	22.35	60.1

Table B3bR.2 - 1° Filtrate chlorinated at variable pH

· pl	i	Turb	Colou	uv	ClDem	Tr	ihalom	ethane:	s (ug/	1)	AOX
Before	After	NTU	Hazen	Abs/m	mg/l	C13	C12Br	ClBr2	Br3	Total	ug/l
5.6 6.0 5.6 6.2 6.4	5.9 6.2 6.8 8.6 9.0	0.1 0.2 0.2 0.2 0.2	1 1 2 1	2.2 2.0 2.1 2.3 2.5	0.71 0.60 0.62 0.55 0.63	4.28 5.49 6.83 8.36 8.13	1.91 2.27 3.00 2.07 1.39	0.87 1.19 0.52		8.66 11.05 10.98	16.9

Table B3bR.3 - Ozonated 1° filtrate chlorinated at variable pH

На	03 Resid	Turb	Colou	uv	ClDem	Tr	ihalom	ethanes	s (ug/	1)	AOX
	mg Cl	NTU	Hazen	Abs/m	mg/l	C13	Cl2Br	ClBr2	Br3	Total	ug/l
5.6 6.3 7.3 8.5 9.2	0.30 0.32 0.03 0.04 0.00	1.3 1.1 0.6 1.0	26 38 24 37 30	4.1 3.5 4.4	0.53 0.47 0.65 0.51 0.53	<0.13 <0.13 2.66 1.43 4.47	0.66 1.73	0.44 1.51 1.23		1.26 6.22 4.63	8.7 8.2 11.2

Table B3bR.4 - Ozonated 1° filtrate chlorinated at pH 9

		Turb	Colou	uv	ClDem	Tr	ihalome	ethanes	ug/:	1)	AOX
pН	Resid mg Cl	NTU	Hazen	Abs/m	mg/l	C13	C12 r	ClBr2	Br3	Total	ug/l
5.4 6.1 7.3 8.4 9.2	0.30 0.32 0.03 0.04 0.00	1.3 1.0 0.6 1.0	26 34 19 32 30	3.7 4.2 3.4 4.3 4.7	0.50 0.29 0.51 0.26 0.53	4.81 5.03 6.18 5.01 4.47	1.15 1.30	0.42 0.38 0.42	<0.03 <0.03 <0.03 <0.03 <0.03	6.80 7.74 6.76	15.6 14.3 12.8 14.6 13.9

PHASE II. TRIAL B3c. EFFECT OF OZONE DISINFECTION (POST OZONATION)

INTRODUCTION

As a result of the trials varying ozone dose and contact time for interfiltration ozonation, it was considered that the best way of applying ozone was to first remove manganese from the water, before applying ozone. Since one filter had been run with no interfiltration oxidant for nearly two months, and this filter had successfully removed manganese during this period, three out of the four 2° RGFs were run with no interfiltration oxidant. The remaining 2° RGF was run as a control, with chlorine applied as the interfiltration oxidant. The three un-oxidised 2° filtrates were then combined and pumped to the ozone contactor, where they were contacted with ozone for about 8 minutes, with an ozone dose of approximately 2 mg/l. The dose was chosen from the results of uv absorbance vs. ozone dose obtained in trial 3a.

RESULTS

Table B3c.1 - Doses and residuals

DATE			8 Apr 9 4 Apr 9					
FERRIC DOSE (mg Fe/l)		1.7						
	New 03	01d 03	New Cl	Old Cl	Dis			
CHLORINE DOSE (mg Cl/1)	_	-	- -	0.57 0.49	-			
OZONE DOSE (mg O3/1)	-	-	- -	-	2.6 1.9			
C1/03 RESIDUAL (mg C1/1 equivalent)	0.00	0.00	0.00	0.13	0.40 0.15			
Mn Interference (mg Cl/l equivalent)	-	-	<u>-</u>	-	0.07			

Table B3c.2 - Colour, uv and turbidity

DETERMINAND	RAW WATER	DAF	1° F 03	RGF Cl	New O3	01d 03		F Old Cl	Dis
рН	5.2 5.2	4.7	6.2 6.5	6.2 6.5	9.0 8.8	8.8 8.8	8.9 8.9	9.0 8.9	7.2 7.2
APPARENT COLOUR (Degrees Hazen)	24 22	16 15	3 1	2 1	3 2	3 2	3 2	3 2	1
TRUE COLOUR (Degrees Hazen)	9 7	2 1	- -	1 1	-	-	-	1 1	-
APPARENT uv (Abs/m)	14.3 13.4	9.0 9.3	3.4	3.4 3.2	3.2 3.5	3.2 3.5	3.4 3.4	3.0 3.1	1.0 1.1
TRUE uv (Abs/m)	8.8	3.5 3.4	- -	- -	-	-	-	-	-
TURBIDITY	1.7	1.0	0.1	0.1	0.1	0.1	0.1	0.1	0.1

Table B3c.3 - Metals

DETERMINAND	RAW WATER	DAF	1°	RGF		2° RGF					
	MATER	DAL	03	Cl	New 03	01d 03	New Cl	Old Cl			
IRON (mg/l)	0.36 0.24	0.93 0.97	0.01	0.02 0.01	0.05 0.05	0.02 0.01	0.05 0.01	0.01 0.01			
MANGANESE (mg/l)	0.18 0.19	0.19 0.20	0.19 0.22	0.19 0.21	0.04	0.01	0.01	0.00			
ALUMINIUM (mg/l)	0.31 0.31	0.22 0.25	0.02 0.03	0.03 0.02	0.03 0.03	0.03	0.03	0.03.			

Table B3c.4 - TOC and bacteriological quality

DETERMINAND	RAW WATER	Hand C	hlorina	ted 2°	RGF	
,	WAIEK	New 03	01d 03	New Cl	Old Cl	Dis
TOC (mg/l)	2.88 2.91	1.47 2.11	1.51 2.00	1.68 1.70	1.55 1.84	1.32 1.70
COLIFORMS TOTAL (per 100ml)	-	0	0 0	0 0	0	0
E-COLI (per 100ml)		0	0	0	0	0
COLONIES 37°C 1-DAY (per ml)	-	0 ` 1	1 4	3 1	1 1	0
COLONIES 22°C 3-DAY (per ml)	-	6 10	5 4	4 18	1 0	10

Table B3c.5 - Non-hand chlorinated samples: disinfection by-products

		2° F	RGF		Dis	Dis
DETERMINAND	New 03	01d 03	New Cl	Old Cl	Feed	Outlet
C13	<0.13	<0.13	<0.13	<0.13	-	<0.13
(ug/1)	<0.13	<0.13	<0.13	<0.13	-	
C12 Br	<0.01	<0.01	<0.01	<0.01	-	<0.01
(ug/l)	<0.01	<0.01	<0.01	<0.01		<0.01
Cl Br2	<0.05	<0.05	<0.05	<0.05	1	<0.05
(ug/l)	<0.05	<0.05	<0.05	<0.05		<0.05
Br3	<0.03	<0.03	<0.03	<0.03	-	<0.03
(ug/l)	<0.03	<0.03	<0.03	<0.03		<0.03
Total THMs (ug/l)	<0.22 <0.22	<0.22 <0.22	<0.22 <0.22	<0.22 <0.22	-	<0.22 <0.22
AOX	-	-	-	21.6	9.6	<8

Dis: Post ozonation contactor

Table B3c.6 - Hand chlorinated samples: disinfection by-products

-	RAW	1° F	RGF		2° F	RGF		Dis	Dis
DETERMINAND	WATER	03	Cl	New 03	01d 03	New Cl	Old Cl	Feed	Outlet
C13 (ug/1)	21.43 24.06	3.91 5.03	3.81 4.72	- 6.09	5.43 6.68	4.97 6.07	7.06 6.63	- •	0.51 1.31
Cl2 Br (ug/l)	0.20 0.35	<0.01	<0.01	0.31	0.27 0.39	0.24	0.33 0.49	-	<0.01 0.16
Cl Br2 (ug/l)	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	- <0.05	<0.05 <0.05	<0.05 <0.05	<0.05 <0.05	- -	<0.05 <0.05
Br3 (ug/l)	<0.03	<0.03 <0.03	<0.03	- <0.03	<0.03 <0.03	<0.03 <0.03	<0.03 <0.03	-	<0.03 <0.03
Total THMs (ug/1)	21.71 24.49	4.00 5.19	3.90 4.86	6.48	5.78 7.15	5.29 6.44	7.47 7.20	–	0.60 1.55
AOX	64.7	29.3	27.9	-	-	-	30.3	29.4	13.6
Cl Demand (mg/l)	0.74	0.28	0.25 0.26	0.27 0.36	0.34 0.29	0.36 0.27	0.62 0.60	0.27	0.36

Table B3c.7 - Mutagenic activity (dose-response slope value)

AC	TIVITY	Inter Filter Cl	No Inter	Filtration O	xidant
		and Hand Chlorination		Post + Ozonation	Post + Ozonation + Hand Cl
TA pH	98 2	2.60	0.86	0.46	0.40
TA pH	98 7	3.22	1.63	0.03	0.54
TA pH	100 2	15.46	0.82	0.01	9.15
TA pH	100 7	11.88	0.94	-0.07	3.80

Negative value indicates a negative slope, i.e. notional anti-mutagenic action.

PHASE II. TRIAL 4. EFFECT OF DUAL POINT OZONATION

PILOT PLANT CONTROL

There were some problems with pH control of the 2° filters. Where this resulted in low pH, caustic was dosed in the lab, before hand chlorination, to increase the pH to 9.0.

Table B4.1 - Doses and residuals

DATE	FERRIC DOSE		OZONE DOSE		INT C1 DOSE		03 RE:	SIDUAL	Cl RE	Cl RESIDUAL		
	Trial mg/l	Cont mg/l	Pre mg/l	Inter mg/l	New mg/l	Old mg/l	New Cl eq	Old Cl eq	New mg/l	Old mg/l		
1 May 90 9 May 90 15 May 90 22 May 90 30 May 90 6 Jun 90	1.7 1.5 1.9 1.9 2.1	2.1 2.0 1.9 1.9 2.5 1.6	1.1 0.8 1.8 1.4 0.4 0.5	0.9 0.8 0.5 0.5 1.7	0.00 0.00 0.00 0.00 0.00	0.48 0.38 0.44 0.42 0.39 0.41	0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 0.00 0.01 0.01	0.00 0.00 0.00 0.00 0.00	0.00 0.10 0.08 0.09 0.07 0.06		

Cl eq:DPD colour (corrected for manganese) equivalent to a chlorine residual, i.e. a check on the presence of ozone

Table B4.2 - pH

OZONE DOSE	RAW	D Z	A F	1°	RGF	03 2	° RGF	Cl 2° RGF		
Pre/ Inter		Trial	Cont	Trial	Cont	New	Old	New	Old	
50/50 50/50 80/20 80/20 20/80 20/80	5.2 5.2 5.2 5.2 5.4 5.4	4.6 4.7 4.6 4.7 4.6 4.8	4.7 4.6 4.4 4.8 4.7 4.6	6.4 6.8 6.4 7.0 6.6 6.6	6.4 6.6 6.4 6.8 6.6 6.5	8.6 9.2 8.6 9.2 8.8 8.9	8.2 9.1 8.4 9.2 8.8 8.9	7.4 8.8 9.0 9.2 9.0 8.9	7.2 9.1 8.9 9.3 9.0	

Table B4.3 - Colour: $^{\circ}$ Hazen (= Abs/m @400nm * 11)

OZONE DOSE	RAW	RAW WATER		TRIAL DAF		CONTROL DAF		1° RGF		° RGF	Cl 2° RGI	
Pre/ Inter	App	True	App	True	App	True	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	23 25 25 24 24 24	7 7 5 5 5 5	13 15 15 13 12 10	2 2 1 1 1	14 15 16 14 12 15	2 2 2 1 1 2	3 3 2 4 1 2	2 2 2 2 1 3	3 3 3 3 2	4 4 3 5 3	2 3 2 3 2 3	2 2 2 2 1 3

Table B4.4 - uv absorbance (Abs/m)

OZONE	OZONE RAW V		WATER TRIA		CONTROL DAF		1° RGF		03 2° RGF		Cl 2°	RGF
Pre/ Inter	App	True	App	True	App	True	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	14.2 14.1 13.1 12.9	7.9 7.8 7.7 7.1 6.9 6.7	8.1 8.4 8.6 7.2 7.2 6.7	3.2 3.1 2.8 2.2 2.6 2.4	8.3 8.4 8.9 8.3 7.3 8.8	3.8 3.2 4.0 3.3 2.6 3.0	3.4 3.5 3.9 2.8 2.9	3.4 2.6 3.5 3.7 2.9 3.7	2.0 2.3 2.7 2.4 1.7	2.2 2.5 2.7 2.5 2.3 1.6	3.5 3.0 3.5 3.7 3.0 3.7	3.1 2.7 3.4 3.2 2.9 3.5

Table B4.5 - Turbidity (NTU)

OZONE	DAM	D A	A F	1°	RGF	03 2	RGF	Cl 2° RGF	
DOSE Pre/ Inter	RAW WATER	Trial	Cont	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	1.9 1.9 1.8 1.8	0.9 1.0 1.2 0.9 0.8 0.6	0.8 1.0 1.2 0.9 0.7 1.0	0.1 0.2 0.2 0.3 0.1 0.1	0.1 0.1 0.1 0.2 0.1 0.2	0.1 0.1 0.1 0.1 0.1	0.1 0.1 0.1 0.1 0.2 0.2	0.1 0.1 0.2 0.1 0.2	0.1 0.1 0.1 0.1 0.1 0.2

Table B4.6 - TOC (mg/1)

OZONE	DAU	03 2°	RGF	C1 2°	RGF
DOSE Pre/ Inter	RAW WATER	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	3.48 3.22 2.79 3.03 3.08 3.09	1.83 1.73 1.67 1.61 1.56 1.75	2.00 1.81 1.70 1.73 1.64 1.79	1.82 2.23 1.87 1.70 1.68 1.69	1.91 1.66 2.13 1.48 1.45 1.74

Table B4.7 - Iron (mg/l)

OZONE DOSE RAW		DAF		1°	RGF	03 2	O3 2° RGF		RGF
Pre/ Inter	WATER	Trial	Cont	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	0.23 0.30 0.36 0.31 0.37 0.34	0.83 0.80 0.91 0.91 0.72 0.58	0.62 0.86 0.68 0.62 0.62 0.69	0.05 0.06 0.10 0.22 0.06 0.10	0.02 0.01 0.03 0.05 0.03 0.12	0.01 0.01 0.04 0.08 0.00 0.02	0.01 0.01 0.05 0.07 0.02 0.02	0.01 0.01 0.02 0.05 0.02 0.09	0.01 0.01 0.03 0.02 0.02 0.02

Table B4.8 - Manganese (mg/l)

OZONE DOSE	RAW	Di	A F	1°	RGF	03 2	° RGF	C1 2	° RGF
Pre/ Inter	1	Trial	Cont	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	0.18 0.18 0.20 0.19 0.20 0.20	0.18 0.18 0.15 0.11 0.20 0.20	0.19 0.20 0.20 0.20 0.21 0.21	0.18 0.26 0.11 0.09 0.20 0.21	0.19 0.28 0.21 0.22 0.20 0.22	0.05 0.04 0.07 0.03 0.05 0.05	0.06 0.05 0.08 0.04 0.07 0.07	0.05 0.01 0.01 0.00 0.01 0.00	0.00 0.00 0.00 0.00 0.00

Table B4.9 - Aluminium (mg/l)

OZONE	RAW	DAF		1° RGF		03 2° RGF		Cl 2° RGF	
Pre/ Inter	WATER	Trial	Cont	Trial	Cont	New	Old	New	Old
50/50 50/50 80/20 80/20 20/80 20/80	L 0.30 0.30 0.26 0.32 0.32	0 0.25 0.29 0.18 0.17 0.15	S 0.21 0.21 0.17 0.16 0.33	T 0.04 0.03 0.05 0.02 0.02	0.02 0.02 0.01 0.02 0.02	L 0.06 0.03 0.04 0.03 0.03	0 0.10 0.03 0.04 0.02 0.03	S 0.02 0.03 0.02 0.03 0.03	T 0.04 0.03 0.02 0.02 0.04

Table B4.10 - Hand Chlorinated Final Water Bacteriological Quality (Total Coliforms, E-Coli (per 100 ml); 37°C 1-Day Colonies, 22°C 3-Day Colonies (per ml)

OZONE	TRIAL	STREAM	CONTROL	STREAM	
DOSE Pre/ Inter	NEW SAND	OLD SAND	NEW SAND	OLD SAND	
50/50 50/50 80/20 80/20 20/80 20/80	0, 0, 3, 5 0, 0, 1,13 0, 0, 4, 6 0, 0, 0, 6 0, 0, 1,10 0, 0, 3, 5	0, 0, 0, 0 0, 0, 0, 13 0, 0, 0, 0 0, 0, 0, 1 0, 0, 0, 1 0, 0, 0, 1	0, 0, 1, 9 0, 0, 1,13 0, 0, 0,10 0, 0, 3, 8 0, 0, 0,19 0, 0, 0, 6	0, 0, 0, 9 0, 0, 0, 5 0, 0, 3, 3 0, 0, 1, 3 0, 0, 0, 6 0, 0, 3,36	

Table B4.11 - Hand chlorinated chloroform (ug/1)

OZONE	DAG	1°	RGF	03 2	RGF	Cl 2	RGF	
DOSE Pre/ Inter	RAW WATER	Trial	Cont	New	Old	New	Old	
50/50 80/20 80/20 20/80	23.07 17.49 22.55 23.08 25.2 16.52	i .	5.25 6.31 5.3		5.52 3.30 1.90 3.06 3.9 <0.13	8.29 6.42 5.45 5.96 6.6 2.72	10.62 7.78 7.47 6.58 7.1 4.27	*

^{*} Analysed at Samlesbury

Table B4.12 - Hand chlorinated bromodichloromethane (ug/l)

OZONE	ID IN EX	1°	RGF	03 2°	RGF	Cl 2° RGF		
DOSE Pre/ Inter	RAW WATER	Trial	Cont	New	Old	New	Old	
50/50 50/50 80/20 80/20 20/80 20/80	0.63 0.36 0.71 0.66 1.4 0.69	0.64 0.46 0.23 1.01 1.3 0.82	0.27 0.23 0.12 0.21 0.4 0.37	0.96 0.29 0.57 0.60 1.0 0.43	0.98 0.30 0.72 0.40 1.0 0.41	0.55 0.53 0.17 0.14 0.8 0.35	0.82 0.56 0.43 0.13 0.6 0.45	

^{*} Analysed at Samlesbury

Table B4.13 - Hand chlorinated dibromochloromethane (ug/1)

OZONE DOSE	RAW	1°	RGF	03 2	° RGF	C1 2	° RGF	
Pre/ Inter	WATER	Trial	Cont	New	Old	New	Old	
	<0.05 <0.05 <0.05	<0.05 0.07 <0.1	<0.05	0.07	0.06	<0.1	0.08 <0.05 <0.05 <0.1	

^{*} Analysed at Samlesbury

Table B4.14 - Hand chlorinated bromoform (ug/1)

OZONE DOSE	RAW	1°	RGF	03 2	° RGF	C1 2	° RGF
Pre/ Inter	WATER	Trial	Cont	New	Old	New	Old
50/50 80/20 80/20 20/80	<0.03 <0.03 <0.03 <0.03 <0.1 <0.03	<0.03 <0.03 <0.03 <0.1	<0.03 <0.03 <0.03 <0.1	<0.03 <0.03 <0.03 <0.1	<0.03 <0.03 <0.03 <0.1	<0.03 <0.03 <0.03 <0.03	<0.03 <0.03 <0.03 <0.03

^{*} Analysed at Samlesbury

Table B4.15 - Hand chlorinated total THMs (ug/l)

								1
OZONE	D 3 52	1°	RGF	03 2°	RGF	Cl 2° RGF		
DOSE Pre/ Inter	RAW WATER	Trial	Cont	New	Old	New	Old	
	23.82 26.8	8.61 5.83 5.41 7.36 7.4 2.79	7.20 4.33 5.45 6.60 5.9 3.17	2.19 3.46 2.34 3.92 4.9 0.81	6.75 3.69 2.96 3.56 5.1 0.77	8.92 7.03 5.70 6.18 7.6 3.15	11.53 8.45 7.98 6.79 7.9 4.80	*

^{*} Analysed at Samlesbury

Table B4.16 - Chlorine demand (mg/1)

OZONE	5357	1°	RGF	03 2°	RGF.		Cl 2°	RGF	
DOSE Pre/ Inter	RAW WATER	Trial	Cont	New	Old	New	O 1 c	l Sa LAB	n d TOTAL
50/50 50/50 80/20 80/20 20/80	0.78	0.37 0.41 0.45 0.44 0.43 0.40	0.31 0.33 0.33 0.31 0.30 0.30	0.37 0.42 0.37 0.36 0.30 0.33	0.33 0.39 0.35 0.33 0.25	0.37 0.35 0.40 0.32 0.37 0.31	0.48 0.28 0.36 0.33 0.32 0.35	0.20 0.14 0.19 0.13 0.17 0.21	0.68 0.42 0.55 0.46 0.49 0.56

Table B4.17 - Hand chlorinated AOX (ug/l)

OZONE DOSE Pre/ Inter	RAW WATER	1° RGF		03 2	° RGF	Cl 2° RGF		
		Trial	Cont	New	Old	New	Old	
50/50 80/20 20/80	68.5	22.5 16.2 20.9	25.4 31.5 27.6	10.1 12.6 11.8	12.9 14.2 8.2	28.4 28.2 28.7	32.0 28.3 30.6	

Table B4.18a- TA 98 Mutagenic activity (slope value)

OZONE DOŠE	OZONATED 2° RGF			CHLORINATED 2° RGF				
Pre/ Int	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND
	рН 2	pH 7	рн 2	рН 7	рН 2	рн 7	рн 2	рН 7
50/50	1.23	1.05	1.67	1.11	3.83	4.31	2.62	4.41

Table B4.18b - TA 100 Mutagenic activity (slope value)

OZONE DOSE	OZ	ONATED	2°	RGF	CHLO:	RINATE) 2° RGF	
Pre/ Int	NEW	SAND	OLD	SAND	NEW	SAND	OLD	SAND
	рН 2	рН 7	рн 2	рН 7	рн 2	рН 7	рн 2	рН 7
50/50	12.66	5.90	13.21	5.67	19.41	14.35	20.16	15.20